

# PROBLEM SET 1 - SOLUTION

DAVID'S EXTRAVAGANT NOTATION: I use an upper comma (') as my decimal symbol. So  $1'35 \text{ m/s}$  means  $1.35 \text{ m/s}$

-PROBLEM N° 1:

a)

Dependent variable  $\rightarrow W$

Independent variables  $\rightarrow A, \rho, U$

Fundamental magnitudes involved: length, time, mass. Use 3 of the variables of the problem to define length, time, and mass scales:

$$\text{LENGTH SCALE} \rightarrow l_{ed} = \sqrt{A}$$

$$\text{TIME SCALE} \rightarrow t_{ed} = \frac{\sqrt{A}}{U}$$

$$\text{MASS SCALE} \rightarrow m_{ed} = \rho A^{3/2}$$

Express the remaining variable/s (in this case just  $W$ ) in terms of  $l_{ed}$ ,  $t_{ed}$ , and  $m_{ed}$ :

$$\text{DIMENSIONS OF } W \rightarrow [W] = \text{force} = m_{ed} \frac{l_{ed}}{t_{ed}^2} = (\rho A^{3/2}) \frac{\sqrt{A}}{(\frac{\sqrt{A}}{U})^2} = \rho A U^2$$

This leads to the dimensionless number  $\Pi = \frac{W}{\rho A U^2}$ . Since

we have only one dimensionless number, it must be constant (There are no other dimensionless numbers it can depend on), i.e.,

$$\Pi = C = \text{constant} \Rightarrow \frac{W}{\rho A U^2} = C \Rightarrow \underline{\underline{W = C \rho A U^2}}$$

b)

$$V = \frac{100}{9.77} \approx 10 \text{ m/s}$$

$$A_{\text{foot}} \approx 30 \times 8 \text{ cm} = 240 \text{ cm}^2 = 2.4 \cdot 10^{-2} \text{ m}^2$$

$$\rho_{\text{water}} = 1000 \text{ kg/m}^3$$

$$G = 1 \text{ (by assumption)}$$

$$W \approx 1000 \cdot 2.4 \cdot 10^{-2} \cdot 10^2 = 2400 \text{ N} > \text{Asafa Powell's weight} \Rightarrow$$

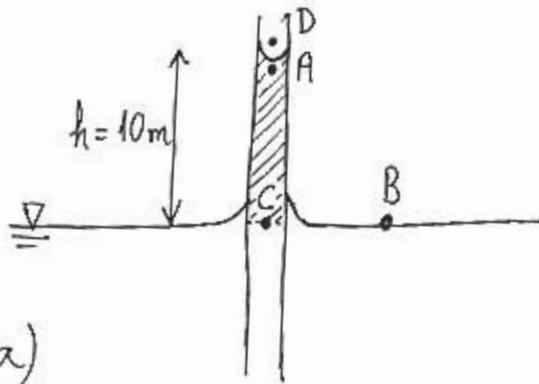
$$(\approx 90 \cdot 9.8 \approx 900 \text{ N})$$

$\Rightarrow$  He would be able <sup>mass · g</sup> to run on water (!)

c)

Certainly the result doesn't seem very realistic. The reason why humans cannot run on water is that the shape of our feet is very different from the basilisk lizard's, and they cannot exert as much thrust. The application of the formula deduced in (a) to part (b) is not correct because in the analysis we have neglected a relevant variable: The foot shape.

- PROBLEM N°2 :

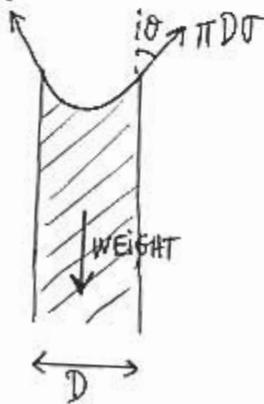


a)

$p_D = p_{ATM}$  and  $p_B = p_{ATM}$ , since they are in contact with the atmosphere.

$p_B = p_C$ , since they are at the same height within a static fluid.

Therefore,  $p_D = p_C$ . Thus, the weight of the shaded water cylinder must be supported by the surface tension force:

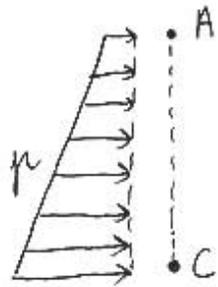


$$\underbrace{\rho g \frac{\pi D^2}{4} h}_{\text{WEIGHT}} = \underbrace{\pi D \sigma \cos \theta}_{\text{SURF. TENSION}} \Rightarrow D = \frac{4 \sigma \cos \theta}{\rho g h}$$

Water at 20°C →  $\begin{cases} \theta \approx 0 \text{ (water in contact with clean glass)} \\ \sigma = 7.28 \cdot 10^{-2} \text{ N/m (Table B.2 in the book)} \end{cases}$

$$\underline{\underline{D}} = \frac{4 \cdot 7.28 \cdot 10^{-2} \cdot 1}{1000 \cdot 9.8 \cdot 10} = 2.97 \cdot 10^{-6} \text{ m} \approx \underline{\underline{3 \mu\text{m}}}$$

b) Pressure between A and C is hydrostatic. Therefore:



$$\begin{aligned} \underline{p_{A, abs}} &= p_{C, abs} - \rho g h = p_{ATM, abs} - \rho g h = \\ &= 101300 - 1000 \cdot 9.8 \cdot 10 = \underline{\underline{3300 \text{ Pa}}} \end{aligned}$$

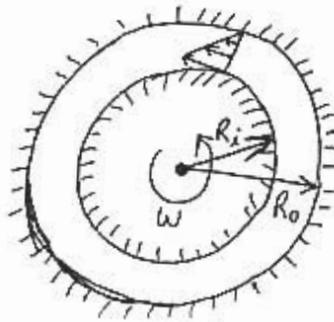
(Note that this is an ABSOLUTE pressure!)

According to Table B.2 in the book, the vapor pressure for water at  $20^\circ\text{C}$  is

$$\underline{\underline{p_v = 2338 \text{ Pa (abs)}}}$$

$$p_{A, abs} > p_v \Rightarrow \underline{\underline{\text{No cavitation}}}$$

- PROBLEM N°3 :



a)

Assume the velocity to vary linearly, i.e.,

$$v = a + b r \quad , \quad R_i \leq r \leq R_o$$

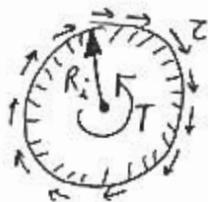
No-slip boundary conditions:

$$\left. \begin{aligned} v(r=R_i) &= \omega R_i \Rightarrow a + b R_i = \omega R_i \\ v(r=R_o) &= 0 \Rightarrow a + b R_o = 0 \end{aligned} \right\} \begin{aligned} a &= \frac{\omega R_i}{R_o - R_i} R_o \\ b &= -\frac{\omega R_i}{R_o - R_i} \end{aligned}$$

Assume Newtonian fluid:

$$\tau = \mu \frac{\partial v}{\partial r} \quad ; \quad \frac{\partial v}{\partial r} = b = -\frac{\omega R_i}{R_o - R_i} \Rightarrow \tau = -\mu \frac{\omega R_i}{R_o - R_i}$$

Balance between the torque,  $T$ , and the moment exerted by the fluid on the cylinder:



$$T = \underbrace{|\tau| \cdot 2\pi R_i l}_{\text{force}} \cdot \underbrace{R_i}_{\text{arm}} = \frac{2\pi R_i^3 l \omega}{R_o - R_i} \mu$$

Check dimensions ( $L$  = length,  $\gamma$  = time,  $M$  = mass):

$$\begin{aligned} [T] &= \frac{ML^2}{\gamma^2} \quad ; \quad \left[ \frac{2\pi R_i^3 l \omega}{R_o - R_i} \mu \right] = \frac{[R_i]^3 [l] [\omega]}{[R_o - R_i]} [\mu] = \frac{L^3 \cdot L \cdot \gamma^{-1} M}{L} \cdot \frac{M}{L \gamma} = \\ &= \frac{ML^2}{\gamma^2} \quad \checkmark \end{aligned}$$

$$b) \mu = \frac{T(R_o - R_i)}{2\pi R_i^3 l \omega} = \frac{T(0.06 - 0.059)}{2\pi (0.059)^3 0.25 \omega} = 3.100 \frac{T}{\omega}$$

$T$  in N·m  
 $\omega$  in  $s^{-1}$   
 $\mu$  in  $\frac{N \cdot s}{m^2}$

$T$ (N·m)	$\omega$ ( $s^{-1}$ )	$\mu$ ( $\frac{N \cdot s}{m^2}$ )
0.178	1.0	0.552
0.353	2.0	0.547
0.536	3.0	0.554
0.715	4.0	0.554
0.880	5.0	0.546
1.066	6.0	0.551

The best estimate of  $\mu$  is the mean value:

$$\bar{\mu} = \frac{\sum_{i=1}^n \mu_i}{n} = 0.551 \frac{N \cdot s}{m^2}$$

c) The standard deviation is

$$\sigma_{\mu} = \sqrt{\frac{1}{n-1} \sum_{i=1}^n (\mu_i - \bar{\mu})^2} \approx 3.5 \cdot 10^{-3} \frac{N \cdot s}{m^2}$$

$\uparrow$  (or  $\frac{1}{n}$ )

Assuming the measurement error to be normally distributed, there is a 95% chance that the "true" value of  $\mu$  is within  $[\bar{\mu} - 2\sigma_{\mu}, \bar{\mu} + 2\sigma_{\mu}]$ . Therefore, we can write

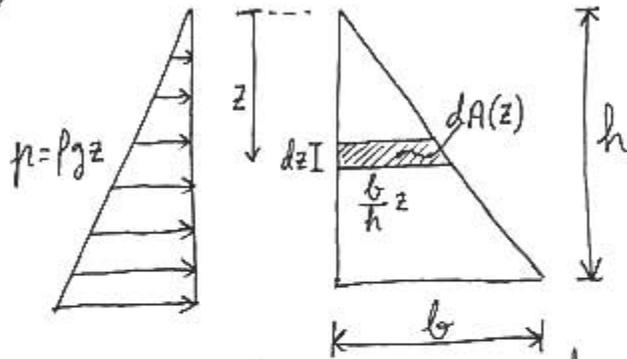
$$\underline{\underline{\mu = 0.551 \pm 0.007 \frac{N \cdot s}{m^2}}}$$

d)

From Figure B.1 in Young et al., at 15°C, fluid is likely SAE 30W oil.

- PROBLEM N° 4:

a)



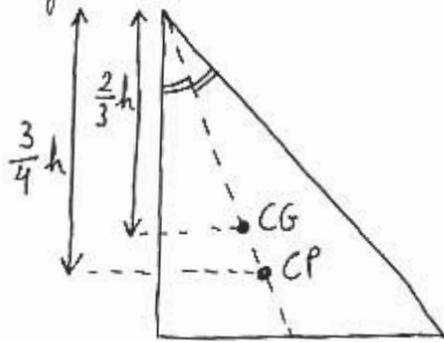
$$\begin{aligned} \text{PRESSURE FORCE} = \underline{F_P} &= \int_0^h p(z) dA(z) = \int_0^h \rho g z \frac{b}{h} z dz = \\ &= \frac{\rho g b}{h} \int_0^h z^2 dz = \frac{\rho g b}{h} \frac{h^3}{3} = \underline{\underline{\frac{1}{3} \rho g b h^2}} \end{aligned}$$

$$\begin{aligned} \text{CENTER OF PRESSURE} \rightarrow \underline{z_{CP}} &= \frac{\int_0^h z p(z) dA(z)}{F_P} = \frac{\frac{\rho g b}{h} \int_0^h z^3 dz}{F_P} = \\ &= \frac{\frac{1}{4} \rho g b h^3}{\frac{1}{3} \rho g b h^2} = \underline{\underline{\frac{3}{4} h}} \end{aligned}$$

$$\text{CENTER OF GRAVITY} \rightarrow \underline{z_{CG}} = \frac{\int_0^h z dA(z)}{\int_0^h dA(z)} = \frac{\frac{1}{3} b h^2}{\frac{1}{2} b h} = \underline{\underline{\frac{2}{3} h}}$$

As for the horizontal location of CP (and CG), since the pressure is constant in the horizontal direction, it (they) must lie on the bisectrix of the upper angle of the triangle.

Therefore

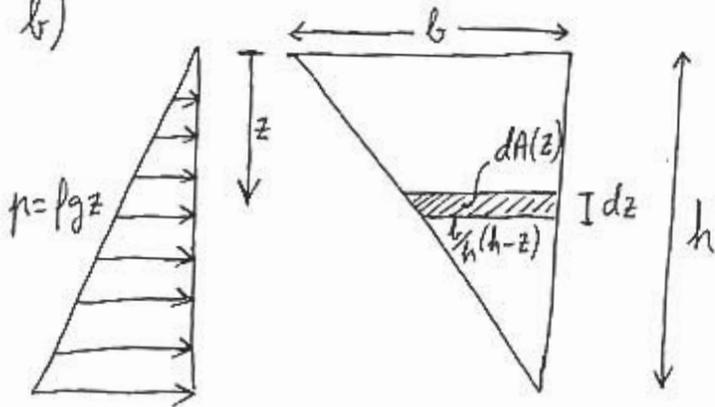


$$CP \neq CG$$

The CP is below the CG.

This makes sense, since pressure increases with depth.

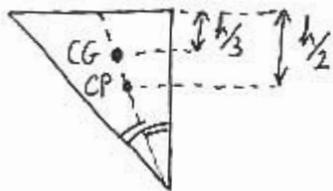
b)



Similarly,

$$F_p = \int_0^h \rho g z \frac{b}{h} (h-z) dz = \frac{\rho g b}{h} \int_0^h z(h-z) dz = \frac{\rho g b}{h} \left( \frac{h^3}{2} - \frac{h^3}{3} \right) = \frac{1}{6} \rho g b h^2$$

$$z_{CP} = \frac{\frac{\rho g b}{h} \int_0^h z^2 (h-z) dz}{\frac{1}{6} \rho g b h^2} = \frac{\frac{\rho g b}{h} \left( \frac{h^4}{3} - \frac{h^4}{4} \right)}{\frac{1}{6} \rho g b h^2} = \frac{h}{2} \quad ; \quad z_{CG} = \frac{h}{3}$$

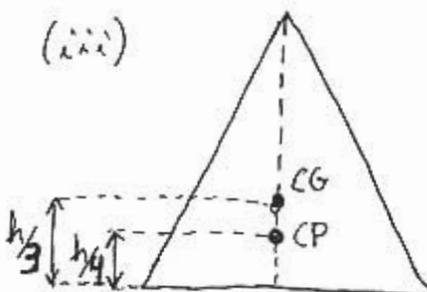


CP below CG

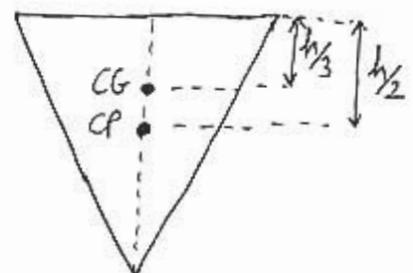
c)

The calculations for (iii) and (iv) are, the same as for (i) and (ii), respectively! So:

(iii)

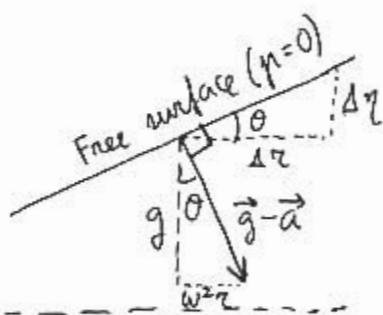
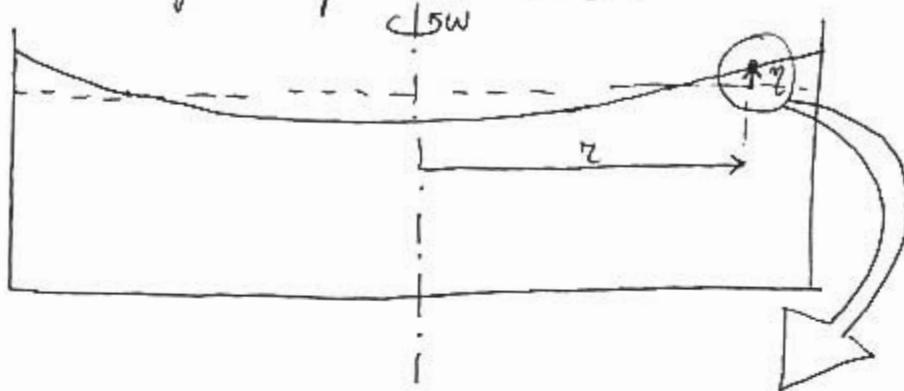


(iv)



- PROBLEM N° 5

The fluid in the centrifuge rotates as a solid body (once in steady state), experiencing a centripetal acceleration of magnitude  $\omega^2 r$ .



Recall from RECIT. 1 that  $\vec{g}-\vec{a} \perp$  Surface of constant  $p$

From the sketch above,

$$\tan \theta = \frac{\Delta \eta}{\Delta r} \quad \text{and} \quad \tan \theta = \frac{\omega^2 r}{g}$$

In the limit of  $\Delta r \rightarrow 0$ ,

$$\frac{d\eta}{dr} = \frac{\omega^2 r}{g} \Rightarrow \int_{\eta_0}^{\eta} d\eta' = \frac{\omega^2}{g} \int_0^r r' dr' \Rightarrow \eta = \eta_0 + \frac{\omega^2 r^2}{2g}$$

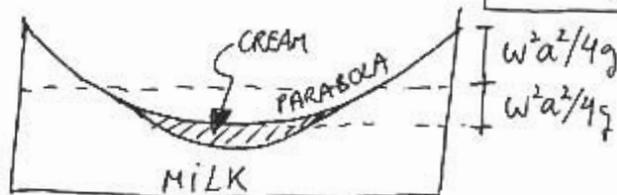
where  $\eta_0$  is a constant that we can determine by imposing that the volume of fluid in the centrifuge remains unchanged.

CHANGE OF VOLUME (with respect to fluid in repose) =  $\Delta V = \int_0^a \eta \cdot 2\pi r dr = \int_0^a \left( \eta_0 + \frac{\omega^2 r^2}{2g} \right) 2\pi r dr =$

$$= 2\pi \left( \eta_0 \frac{a^2}{2} + \frac{\omega^2}{2g} \frac{a^4}{4} \right) \text{ must be } 0 \Rightarrow$$

$$\Rightarrow \eta_0 = -\frac{\omega^2}{4g} a^2 \Rightarrow \eta_0 = -\frac{\omega^2 a^2}{4g} \text{ and } \boxed{\eta = \frac{\omega^2}{2g} \left( r^2 - \frac{a^2}{2} \right)}$$

$$\eta(r=a) = \frac{\omega^2 a^2}{4g}$$



The cream is lighter than the milk, so it will tend to concentrate in the upper center region (Effective gravity,  $\vec{g} - \vec{a}$ , is directed towards the bottom and the edges).

#### ALTERNATIVE METHOD:

From Recitation 1,  $\vec{\nabla} p = \rho(\vec{g} - \vec{a})$ , where  $\vec{\nabla} p = \left( \frac{\partial p}{\partial r}, \frac{\partial p}{\partial z} \right)$

$$\vec{a} = (-\omega^2 r, 0), \vec{g} = (0, -g)$$

Therefore,

$$\left. \begin{aligned} \frac{\partial p}{\partial r} &= \rho(0 - (-\omega^2 r)) = \rho \omega^2 r \Rightarrow p = \rho \omega^2 \frac{r^2}{2} + f_1(z) + G_0 \\ \frac{\partial p}{\partial z} &= \rho(-g - 0) = -\rho g \Rightarrow p = -\rho g z + f_2(r) + G_0 \end{aligned} \right\} \Rightarrow$$

$$\Rightarrow p = -\rho g z + \rho \frac{\omega^2 r^2}{2} + G_0, \text{ where } G_0 \text{ is a constant.}$$

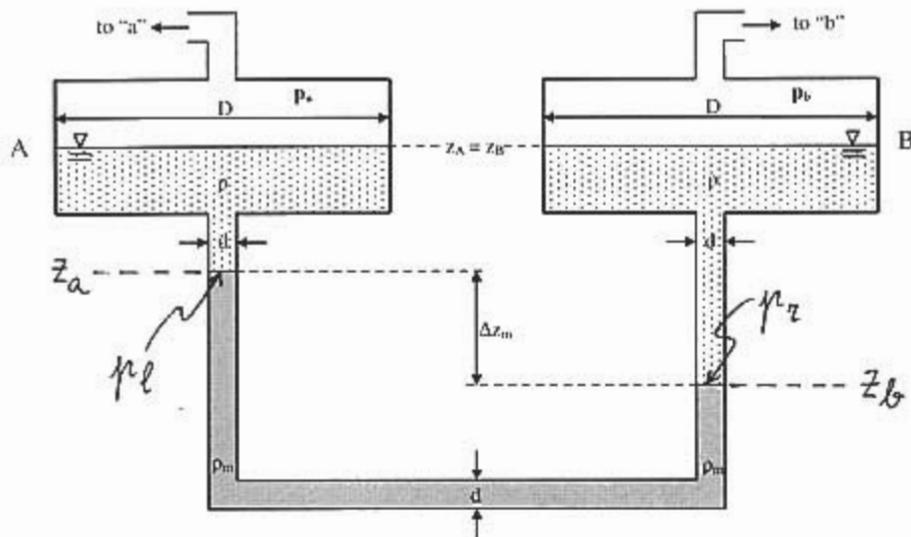
Since  $p=0$  at  $z=r$ ,

$$-\rho g r + \rho \omega^2 \frac{r^2}{2} + G_0 = 0$$

$$r = \frac{G_0}{\rho g} + \frac{\omega^2 r^2}{2g}$$

Same as before, if you rename the constant  $\frac{G_0}{\rho g} = \eta_0$ .

- PROBLEM N° 6:



- a) From chamber A, where  $p = p_a$ , to surface of manometer fluid at  $z = z_a$  and  $p = p_l$

$$p_a + \rho g z_A = p_l + \rho g z_a \quad (1)$$

- From chamber B, where  $p = p_b$ , to surface of manometer fluid at  $z = z_b$  and  $p = p_r$

$$p_b + \rho g z_B = p_r + \rho g z_b \quad (2)$$

Combining (1) and (2) we obtain, since  $z_A = z_B$ ,

$$p_b - p_a = \Delta p = \rho g (z_b - z_a) + p_r - p_l \quad (3)$$

Within manometer fluid  $p + \rho_m g z = \text{constant}$ , so

$$p_l + \rho_m g z_a = p_r + \rho_m g z_b \Rightarrow p_r - p_l = -\rho_m g (z_b - z_a) \quad (4)$$

which can be introduced in (3) to obtain

$$\Delta p = p_b - p_a = \rho g (z_b - z_a) - \rho_m g (z_b - z_a) = -(\rho_m - \rho) g (z_b - z_a)$$

or, with  $\Delta z_m = z_a - z_b$

$$\underline{\underline{\Delta p = (\rho_m - \rho) g \Delta z_m}}$$

b)

Rearranging result above

$$\Delta z_m = \frac{\Delta p}{(\rho_m - \rho) g}$$

For  $\Delta p = 1 \text{ Pa} = 1 \text{ N/m}^2$ ,  $\rho_m = 13'6 \rho$  and  $\rho = 10^3 \text{ kg/m}^3$ , and  $g \approx 10 \text{ m/s}^2$

$$\Delta z_m = \frac{1}{(13'6 - 1) \cdot 1000 \cdot 10} \approx 0'8 \cdot 10^{-5} \text{ m} < 0'01 \text{ mm}$$

Impossible to read this manometer!

For  $\Delta p = 1 \text{ Pa}$ ,  $\rho_m = 1'025 \rho$ ,  $\rho = 10^3 \text{ kg/m}^3$ , and  $g \approx 10 \text{ m/s}^2$

$$\Delta z_m = \frac{1}{(1'025 - 1) \cdot 1000 \cdot 10} \approx 4 \cdot 10^{-3} \text{ m} = 4 \text{ mm}$$

This could be read (with some effort)

Use  $\rho_m = 1025 \text{ kg/m}^3$  manometer fluid

c)

If  $D \gg d$  the levels in chambers A and B will not change significantly when  $\Delta p = p_b - p_a$  changes, i.e.,  $z_A = z_B$  remains true regardless of  $\Delta p$ .

## Comments about Problem Set 1

### PROBLEM 1:

- There were many different answers to part (c). Some groups argued that the reason for the unexpected ability of Asafa Powell to run on water was that Asafa and the lizard have a different ratio of weight ( $W$ ) to feet sole area ( $A$ ) (since the area increases with  $L^2$  and the weight with  $L^3$ ). This argument is not correct: Both parameters  $W$  and  $A$  have been included in the analysis, and therefore it doesn't matter if their ratio changes. The key to part (c) was thinking of which variables had **not** been included in the analysis.

### PROBLEM 2:

- Some groups stated that the absolute pressure at point A is equal to atmospheric. This is not true: the absolute pressure in the fluid is atmospheric 10 meters below A, so the absolute pressure in A is smaller than atmospheric. How can this be possible if the pressure of the air slightly above A is atmospheric? This is due to surface tension effects. The surface tension introduces a force on the surface of the fluid, which causes a discontinuity between the pressure in the air and the pressure in the fluid below the surface. So why do we usually take  $p_{\text{abs}}=p_{\text{atm}}$  at the surface of a body of water in contact with the atmosphere? Because surface tension effects are only relevant very close to the surface boundaries, and we usually have a free surface of a size much larger than the cross-section of a capillary tube.

- Remember that  $1\text{kN} = 1000\text{ N}$ , and  $1\text{ N} = 0.001\text{ kN}$ . For some reason, some people got confused with this twice in the problem, and obtained a tube diameter 1 million times larger than the correct one (which you should notice!). Be careful when converting units. The numerical value must become smaller (1 to 0.001) when the unit in which you measure becomes larger (N to kN).

### PROBLEM 3:

- Many of you seemed confused about the meaning of the accuracy of an estimate. When you have a series of measurements of an unknown parameter ( $\mu$  in this problem), your best estimate of the true value is the mean, and the accuracy is given in terms of the standard deviation. Assuming the error to be normally distributed (which is generally the case), the most precise way of giving the value of the unknown parameter is as

(value of the parameter) = (mean)  $\pm$  2\*(standard deviation)

where 2\*(standard deviation) is the accuracy of the estimate. Due to the properties of the normal distribution, you can be 95% sure that the true value of the parameter will be within  $\pm 2$  standard deviations about the mean.

## GENERAL COMMENTS:

- In general, we think that you give too little information about how you resolve the problems. It is not enough to write some equations; **you need to show the details of your work and explain in words what you are doing**. Along the same lines, please avoid giving a numerical answer without an explanation of where it comes from. If you don't show your calculations and your numerical answer is wrong, you'll most likely get 0 points in that part. Even if your numerical answer is right, you probably won't get full score, since you are not proving that you know how to do the problem. This also applies to solutions obtained with a spreadsheet (which some people used in problem 3): Show sample calculations, not just a print with the numerical answer! When the answer is qualitative, you also need to explain how you came up with it. For instance, in the centrifuge problem, some groups wrote that the cream ends up at the center, on top of the milk, without any explanation of why this is the case. This is considered an incomplete answer.

- Whenever possible, don't stop working at the numerical answer or final analytical expression. Instead, you can do a number of things to explore the meaning of your result:

- Explain the implications of the result: How does it answer to the question asked in the problem? (E.g., in problem three, part c, some people wrote down the value of the standard deviation... without commenting how it relates to the accuracy of the estimate).
- Check that your solution is dimensionally correct. If your answer is an analytical expression, check that the dimensions of the left and right hand sides are the same. If it is a number, check that the units match the magnitude you are calculating (i.e., a pressure must be in Pa or another pressure unit).
- If it is a numerical answer, comment about its magnitude. Is it big or small? Is it a reasonable value? Did you expect a result of that order of magnitude? (E.g., in problem 2, some people got a diameter of 3 meters... Even if you don't find any mistake in your calculations, you should realize that such a result is unreasonably big and comment about it).
- If your answer is an analytical expression, comment whether the dependencies between variables make sense. (For instance, in problem 3, we expect  $\omega$  to increase with the applied torque, so it would be surprising if  $\omega$  appeared in the denominator of the right hand side of the expression).
- If your answer is an analytical expression, you may be able to analyze particular cases and see if the result makes sense. (E.g., in the centrifuge problem, check for a horizontal surface when  $\omega = 0$ ).
- Represent your solution graphically whenever possible. If it is a vector, plot it. If it is a function, represent it in an x-y diagram or similar. (For instance, represent the free surface in the centrifuge problem)

This kind of analysis will give you insight into the solution. From the grader's point of view, it will be clear that you understand the meaning of your answer (so you may even get some bonus points!).