ICE Module I - Batch Process Development Memo 7

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SUBJECT:	Physical Property Data for Lucretex Components

This memo provides physical property data for all the components in the case-study. Table 1 contains pure-component property values.

Models for Temperature-Dependent Pure-Component Properties (see Table 2)

Ideal Gas Heat Capacity (J kmol⁻¹ K⁻¹):

$$\begin{split} \mathbf{C}_{\text{p,ig}} &= \mathbf{A}_1 + \mathbf{A}_2 \mathbf{T} + \mathbf{A}_3 \mathbf{T}^2 + \mathbf{A}_4 \mathbf{T}^5 + \mathbf{A}_5 \mathbf{T}^4 + \mathbf{A}_6 \mathbf{T}^5 \qquad \mathbf{A}_7 \leq \mathbf{T} \leq \mathbf{A}_8 \\ &= \mathbf{A}_9 + \mathbf{A}_{10} \mathbf{T}^{\mathbf{A}_{11}} \qquad \qquad \mathbf{T} < \mathbf{A}_7 \end{split}$$

Extended-Range Antoine Equation for Vapor Pressure (N m⁻²):

$$\ln P_{s} = B_{1} + \frac{B_{2}}{T + B_{3}} + B_{4}T + B_{5}\ln T + B_{6}T^{B_{7}} \qquad B_{8} \le T \le B_{9}$$

Binary Wilson Model for Activity Coefficients (see Table 3)

The liquid interactions between components i and j are represented by the Wilson liquid solution model in the following form:

$$\begin{split} &\ln \gamma_i = 1 - \mathbf{B}_i - \sum_{j=1}^n e^{a_{jj} + \frac{\mathbf{b}_{ji}}{T} - \mathbf{B}_j} \mathbf{x}_j \\ &\mathbf{B}_i = \ln \Bigg[\sum_{j=1}^n e^{a_{ij} + \frac{\mathbf{b}_{ij}}{T}} \mathbf{x}_j \Bigg] \end{split}$$

where γ_i denotes the activity coefficient of component i, a_{ij} and b_{ij} represent binary interaction parameters between component pairs (i, j), and T denotes the temperature (in kelvins) of the system. All available binary interaction parameters are shown in Table 3.