

2.43 ADVANCED THERMODYNAMICS

Spring Term 2024

LECTURE 03

Room 3-442

Tuesday, February 13, 2:30pm - 4:30pm

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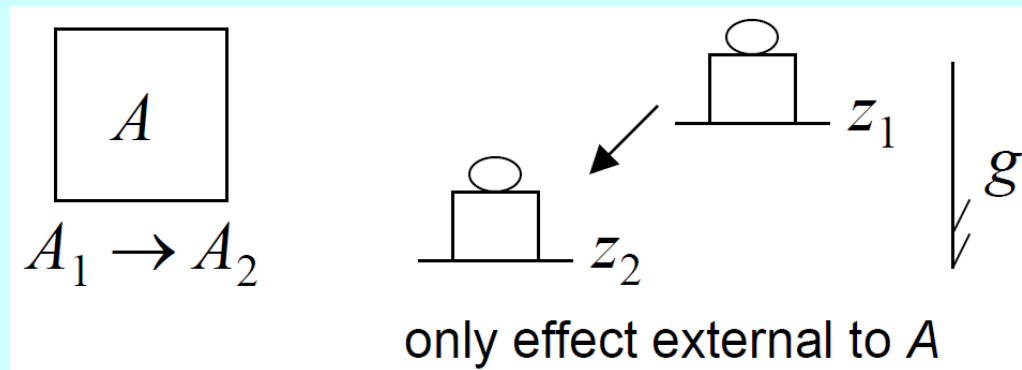
Room 3-351d

Review of basic concepts: **Main consequence of the First Law:**
definition of property Energy

First Law:

Assertion 1: any pair of states A_1 and A_2 with compatible values of the amounts of constituents and the parameters of a (well-defined) system A can always be interconnected by means of a weight process.

Assertion 2: the product $mg(z_2 - z_1)$ assumes the same value for all weight processes that connect the two given states A_1 and A_2 .



The most important consequence of the First Law is that it provides support to the **definition of property energy** for every (well-defined) system A in any state A_1

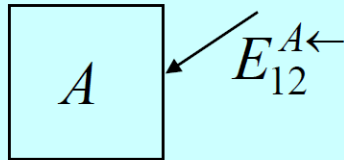
$$E_1^A = E_0^A - mg(z_1 - z_0)$$

where A_0 is a reference state to which we assign the arbitrary value E_0 .

Review of basic concepts: **Consequences of the First Law:**

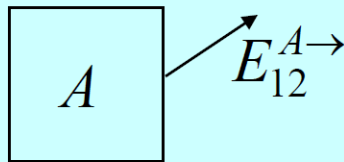
Energy balance equation

Energy balance equation for a process for system A:



$A_1 \rightarrow A_2$

or, equivalently,



$A_1 \rightarrow A_2$

$$E_2^A - E_1^A = E_{12}^{A\leftarrow}$$

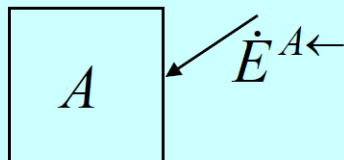
- $E_{12}^{A\leftarrow}$ energy exchanged between A and its environment during the time interval from t_1 to t_2 (if positive, the net transfer is into A)

$E_{12}^{A\leftarrow}$

$$E_2^A - E_1^A = -E_{12}^{A\rightarrow}$$

- $E_{12}^{A\rightarrow}$ energy exchanged between A and its environment during the time interval from t_1 to t_2 (if positive, the net transfer is out of A)

For a continuous process, consider an infinitesimal time interval ($t_1=t$ and $t_2=t+dt$)



$$\frac{dE^A}{dt} = \dot{E}^{A\leftarrow}$$

- $\dot{E}^{A\leftarrow}$ net power, net rate of energy transfer (into A if positive, out of A if negative)

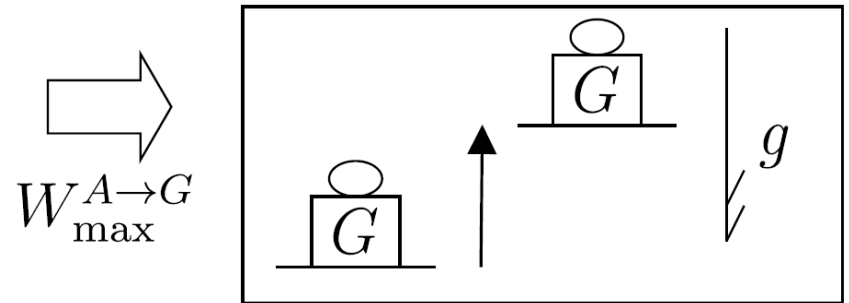
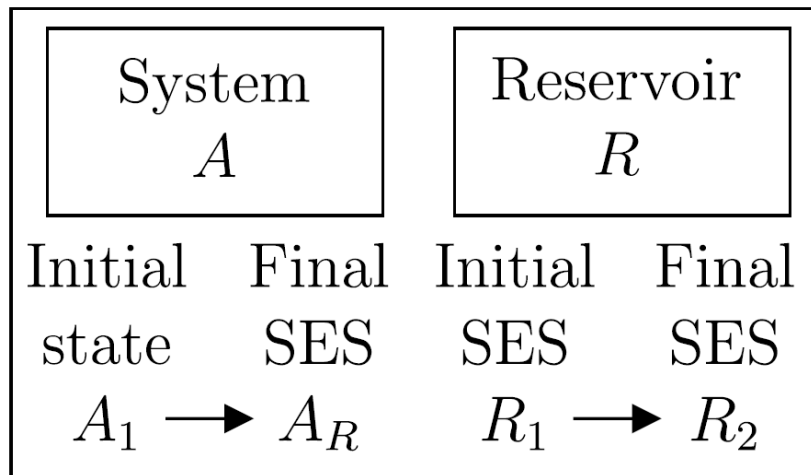
Review of basic concepts: **importance of the second part of the statement of the Second Law of Thermodynamics**

Second Law:

Assertion 1: in the subset of states of a system compatible with given values of the amounts of constituents n and of the parameters β , there is always one and only one SES for each value of the energy E .

Assertion 2: Starting from any state of the system, it is always possible, through a reversible weight process, to reach a SES with arbitrarily fixed, compatible values of the amounts of constituents and the parameters.

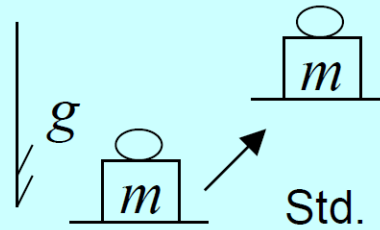
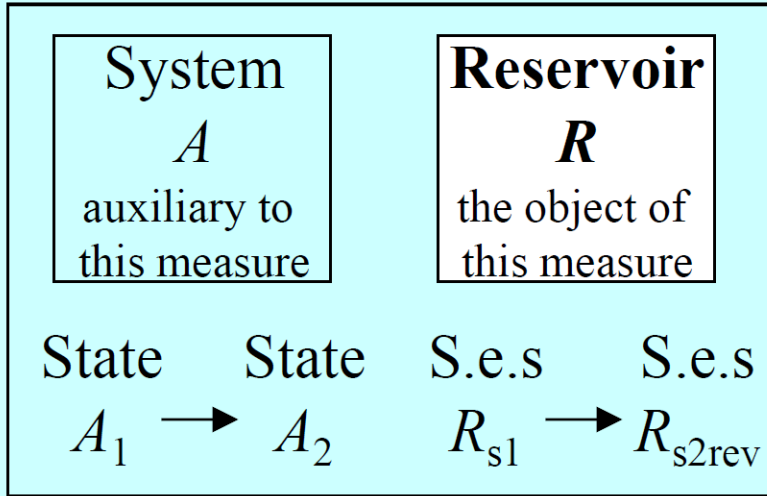
Reversible weight process for AR ending with A and R in MSE



The only effect external to AR is the lifting of a weight

Review of basic concepts: Consequences of the (First&)Second Law:

Measurement procedure defining the “constant temperature of a thermal reservoir”

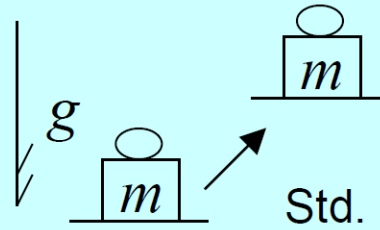
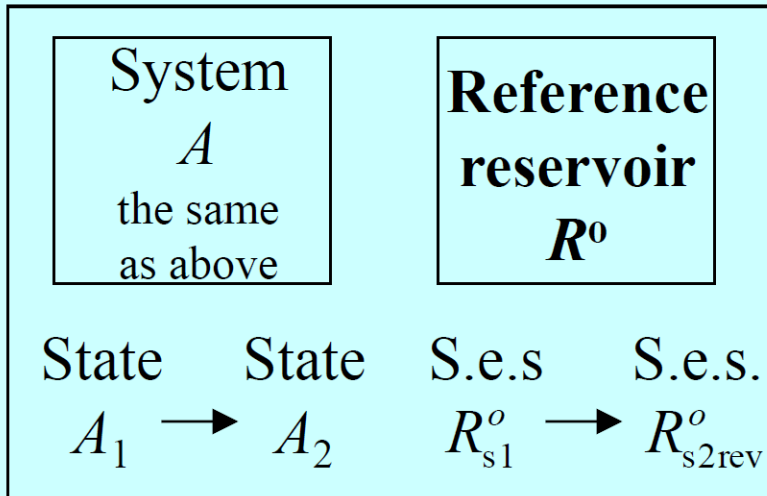


Std. rev. w.p. for AR
 Measure the change in E^R

$$(E_{s2rev}^R - E_{s1}^R)_{A_1 R_{s1} \Rightarrow A_2 R_{s2rev}} \underset{w,rev}{\Rightarrow}$$

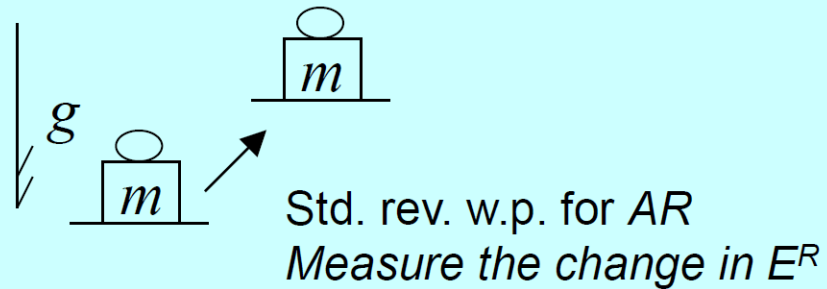
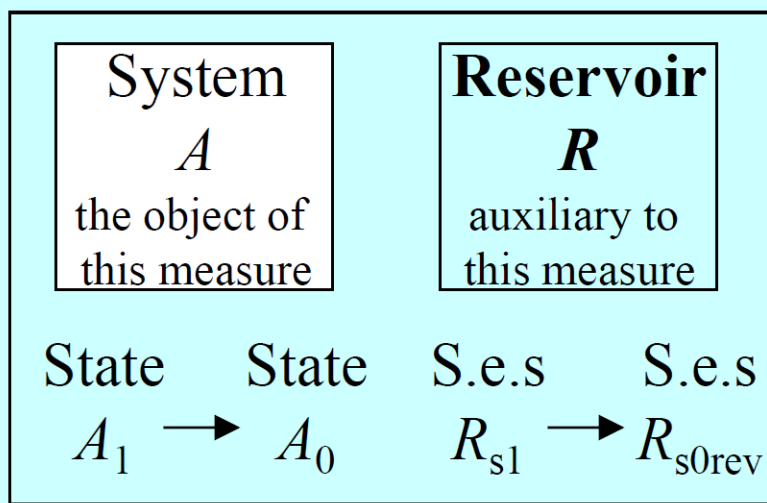
$$(E_{s2rev}^{R^o} - E_{s1}^{R^o})_{A_1 R_{s1}^o \Rightarrow A_2 R_{s2rev}^o} \underset{w,rev}{\Rightarrow}$$

Repeat for the same A_1 and A_2 , but with a reference reservoir R^o (water at the triple point)



Std. rev. w.p. for AR^o
 Measure the change in E^R

Review of basic concepts: **Consequences of the (First&)Second Law:** **definition of property Entropy**



state A_0 is an arbitrarily chosen state to which we assign the arbitrary reference value S_0

The ratio:

$$\frac{(E_{s0rev}^R - E_{s1}^R)_{A_1 R_{s1} \Rightarrow A_0 R_{s0rev} \text{ w.rev}}}{T_R}$$

- is independent of reservoir R and of its initial state R_{s1}
- It depends therefore only on system A and the pair of states A_1 and A_0

Hence it defines a property:

$$S_1 = S_0 + \frac{(E_{s0rev}^R - E_{s1}^R)_{A_1 R_{s1} \Rightarrow A_0 R_{s0rev} \text{ w.rev}}}{T_R}$$

Review of basic concepts: **Consequences of the (First&)Second Law:** **engineering meaning of Entropy**

From the relation

$$\Omega_1^R = (E_1 - E_R) - T_R (S_1 - S_R)$$

We obtain the following interpretation of the physical meaning of entropy:

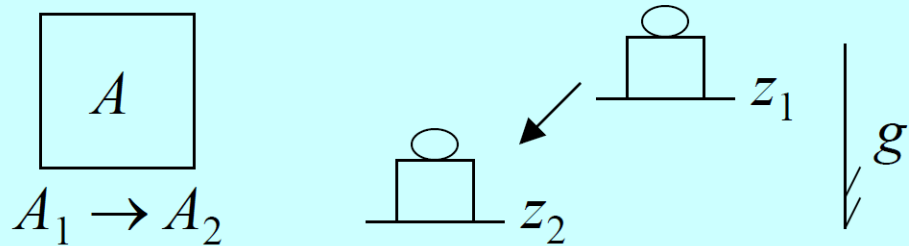
Energy of system A which is unavailable w.r.to reservoir R
(it cannot be given to a weight without other effects)

$$S_1 = \frac{E_1 - \Omega_1^R}{T_R} + S_R - \frac{E_R}{T_R}$$

A constant, independent of the state A_1

So, the entropy is a linear function of that part of the energy of the system which is unavailable with respect to reservoir, the constant of proportionality being the inverse of the temperature of the reservoir.

Review of basic concepts: **Consequences of the (First&)Second Law:**
Theorems on criteria for the reversibility of a weight process



Theorem. The following equivalent conditions are necessary and sufficient for a weight process for system A to be reversible or irreversible:

reversible iff:

$$E_2 - \Psi_2 = E_1 - \Psi_1$$

$$E_2 - \Omega_2^R = E_1 - \Omega_1^R$$

$$S_2 = S_1$$

irreversible iff:

$$E_2 - \Psi_2 > E_1 - \Psi_1$$

$$E_2 - \Omega_2^R > E_1 - \Omega_1^R$$

$$S_2 > S_1$$

impossible iff:

$$E_2 - \Psi_2 < E_1 - \Psi_1$$

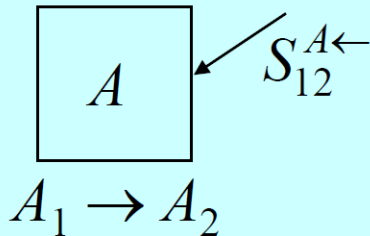
$$E_2 - \Omega_2^R < E_1 - \Omega_1^R$$

$$S_2 < S_1$$

Review of basic concepts: **Consequences of the (First&)Second Law:**
Entropy balance equation

Entropy balance equation for a process for system A:

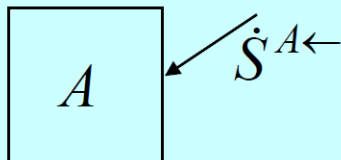
$$S_2^A - S_1^A = S_{12}^{A\leftarrow} + (S_{\text{irr}})_{12}^A$$



- $S_{12}^{A\leftarrow}$ entropy exchanged between A and its environment during the time interval from t_1 to t_2 (if positive, the net transfer is into A)
- $(S_{\text{irr}})_{12}^A \geq 0$ entropy generated by irreversibility within the system during the process (=0 if reversible)

For a continuous process, consider an infinitesimal time interval ($t_1=t$ and $t_2=t+dt$)

$$\frac{dS^A}{dt} = \dot{S}^{A\leftarrow} + (\dot{S}_{\text{irr}})^A$$



- $\dot{S}^{A\leftarrow}$ net rate of entropy transfer (into A if positive, out of A if negative)
- $(\dot{S}_{\text{irr}})^A \geq 0$ rate of entropy generation by irreversibility within the system (=0 if the process is reversible)

Review of basic concepts: **Consequences of the (First&)Second Law:**

Maximum Entropy Principle

and Minimum Energy Principle (except for special systems)

Maximum entropy principle: among all the states with the same given values of the amounts of constituents, the parameters, and the energy, only the stable equilibrium state has the maximum value of the entropy.

(it is a direct consequence of the definition of s.e.s. and the statement of the Second Law; it holds in general for all systems)

A
 n and β fixed

Given the s.e.s. $A_{\text{es}}(E_1)$ with energy E_1 and any **other** state A_1 with the same E_1 , we have:

$$S_1 < S_{\text{es}}(E_1)$$

A_1 $A_{\text{es}}(E_1)$

Minimum energy principle: among all the states with the same given values of the amounts of constituents, the parameters, and the entropy, only the stable equilibrium state has the minimum value of the energy.

(it holds in general for all systems with translational, rotational, and vibrational degrees of freedom, which from any state can receive energy in a w.p.)

(there are 'special' systems -- those that have an upper bound to the energy -- that admit two s.e.s. for every value of the entropy, one with minimum energy and positive temperature and the other with maximum energy and negative temperature)

Review of basic concepts: **Consequences of the (First&)Second Law:**
(Stable equilibrium) **State Principle and Fundamental Relation**

State principle: among all the states with the same given values of the amounts of constituents, the parameters, and the energy, one and only one is a stable equilibrium state (Second Law) and therefore the value of any property is uniquely determined by the values of the amounts of constituents, the parameters, and the energy ($r+s+1$).

$$P = P(E, n_1, \dots, n_r, \beta_1, \dots, \beta_s)$$

Fondamental relation for the s.e.s. (in entropy form): it is the state principle applied to property entropy

$$S = S(E, n_1, \dots, n_r, \beta_1, \dots, \beta_s)$$

Fondamental relation for the s.e.s. in energy form: obtained by solving the above relation to obtain

$$E = E(S, n_1, \dots, n_r, \beta_1, \dots, \beta_s)$$

Taylor series expansion around a s.e.s. :

$$S(E + \Delta E, n, \beta) = S(E, n, \beta) + \left. \frac{\partial S}{\partial E} \right|_E \Delta E + \frac{1}{2} \left. \frac{\partial^2 S}{\partial E^2} \right|_E (\Delta E)^2 + \dots$$

Review of basic concepts:

**Maximum entropy principle,
State principle,
Fundamental relation for the SESs,
Temperature, pressure, and chemical potentials,
Gibbs relation**

Review of basic concepts: **Consequences of the (First&)Second Law:**
Partial derivatives of the fundamental relation
Gibbs relation

Fundamental relation for a system with volume as the only parameter

$$S = S(E, V, n_1, \dots, n_r)$$

Gibbs relation in entropy form

$$dS = \frac{1}{T} dE + \frac{p}{T} dV - \frac{\mu_1}{T} dn_1 - \dots - \frac{\mu_r}{T} dn_r$$

Fundamental relation in energy form

$$E = E(S, V, n_1, \dots, n_r)$$

Gibbs relation

$$dE = TdS - pdV + \mu_1 dn_1 + \dots + \mu_r dn_r$$

Review of basic concepts: **Consequences of the (First&)Second Law:**

Partial derivatives of the fundamental relation

Each partial derivative of the fundamental relation, either in entropy or energy form, represents a property of the family of s.e.s. of the system.

Note = we often consider systems that have volume as the only parameter, therefore, $S=S(E, \mathbf{n}, V)$ and $E=E(S, \mathbf{n}, V)$.

The (*absolute*) *temperature* is defined by

$$T = \left(\frac{\partial E}{\partial S} \right)_{\mathbf{n}, V} \quad \text{or} \quad \left(\frac{\partial S}{\partial E} \right)_{\mathbf{n}, V} = \frac{1}{T}$$

The *chemical potential of the i-th constituent* is defined by

$$\mu_i = \left(\frac{\partial E}{\partial n_i} \right)_{S, \mathbf{n}, V} \quad \text{or} \quad \left(\frac{\partial S}{\partial n_i} \right)_{E, \mathbf{n}, V} = -\frac{\mu_i}{T}$$

The *pressure* is defined by

$$p = -\left(\frac{\partial E}{\partial V} \right)_{S, \mathbf{n}} \quad \text{or} \quad \left(\frac{\partial S}{\partial V} \right)_{E, \mathbf{n}} = \frac{p}{T}$$

Notation for partial derivatives

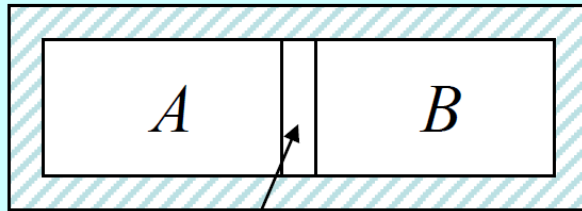
Given the relation $z=z(x,y)$ the symbol

$$\left(\frac{\partial z}{\partial x} \right)_y = \frac{\partial z(x, y)}{\partial x}$$

Contains also the information about what are the other variables of the function being differentiated

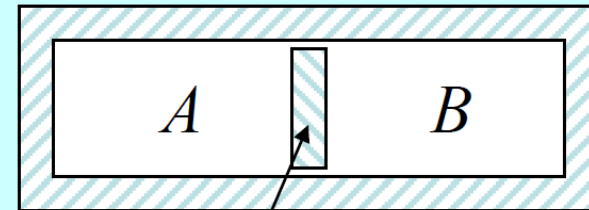
Review of basic concepts: **Consequences of the Maximum Entropy Principle:**
Necessary conditions for mutual equilibrium

Two systems are in *mutual equilibrium* if the respective states are such that the composite system is in a stable equilibrium state.



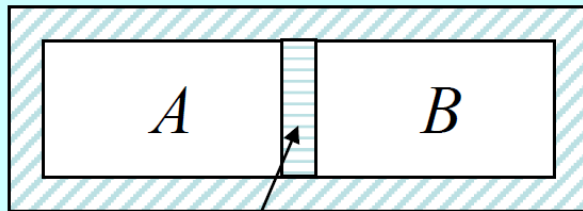
Diathermal wall

- Equality of the **temperatures** of the two systems is a n.c. for m.e. if the two systems can exchange **energy**.



Movable pistone

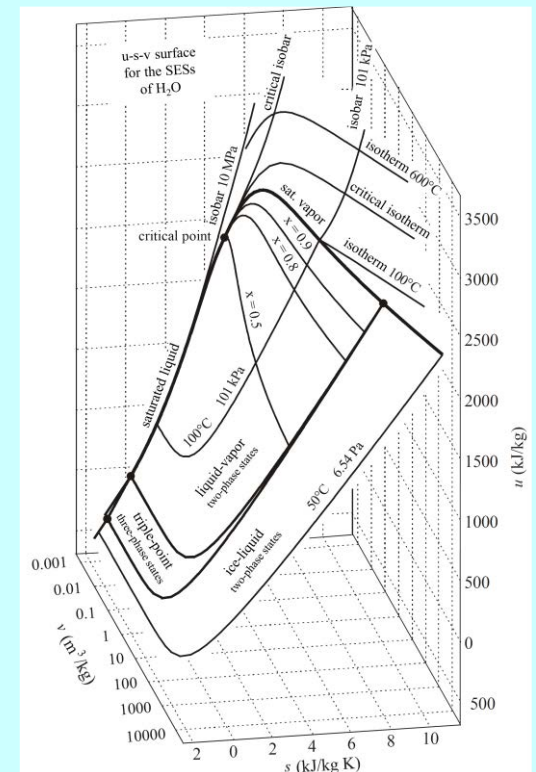
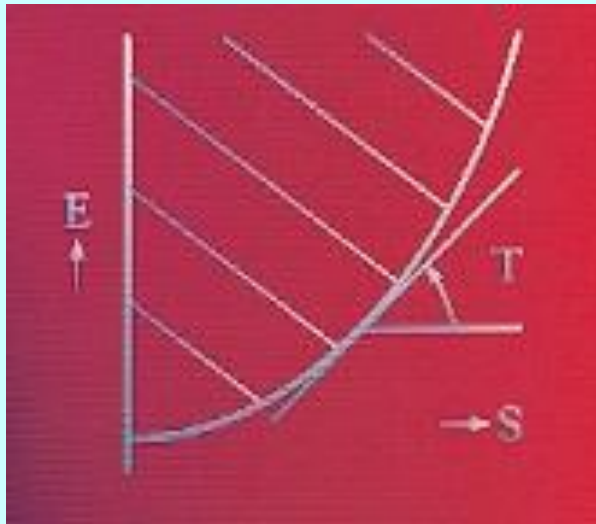
- Equality of the **pressures** of the two systems is a n.c. for m.e. if the two systems can exchange **volume**.



Wall permeable
to the i-th costituent

- Equality of the **chemical potentials of the *i*-th constituent** in the two systems is a n.c. for m.e. if the two systems can exchange **the *i*-th constituent**.

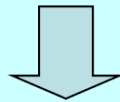
Graphical representation of basic concepts on Energy vs Entropy diagrams



Graphical representation of basic concepts on **Energy vs Entropy diagrams:**

Projection of the state space on the E-S plane

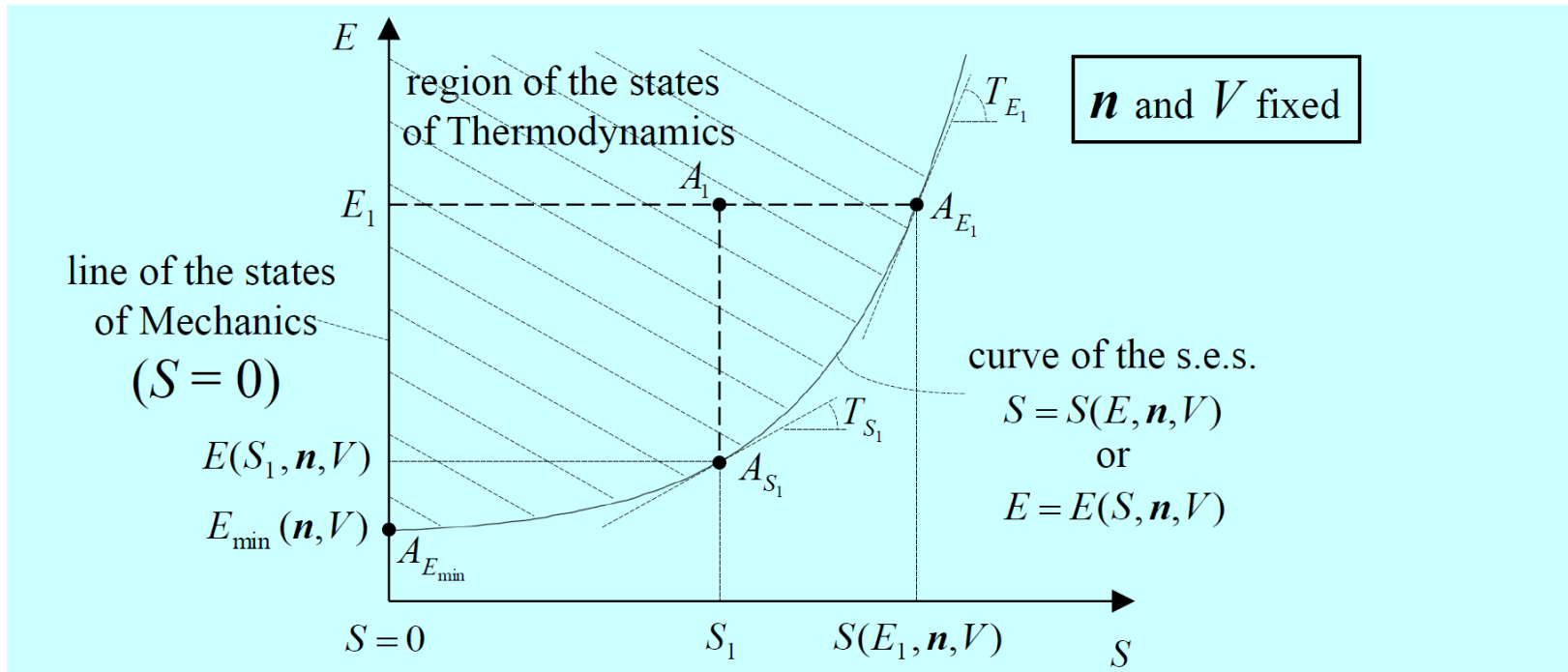
- States are points in a multidimensional space with one axis for every amount, parameter, and independent property (almost always infinite dimensional)
- Consider the subspace corresponding to fixed values of the amounts of constituents and the parameters
- Project all points in this subspace on the two-dimensional energy vs entropy plane



We obtain a 2D representation of all the states of a system with given values of amounts and parameters

Graphical representation of basic concepts on **Energy vs Entropy diagrams:**

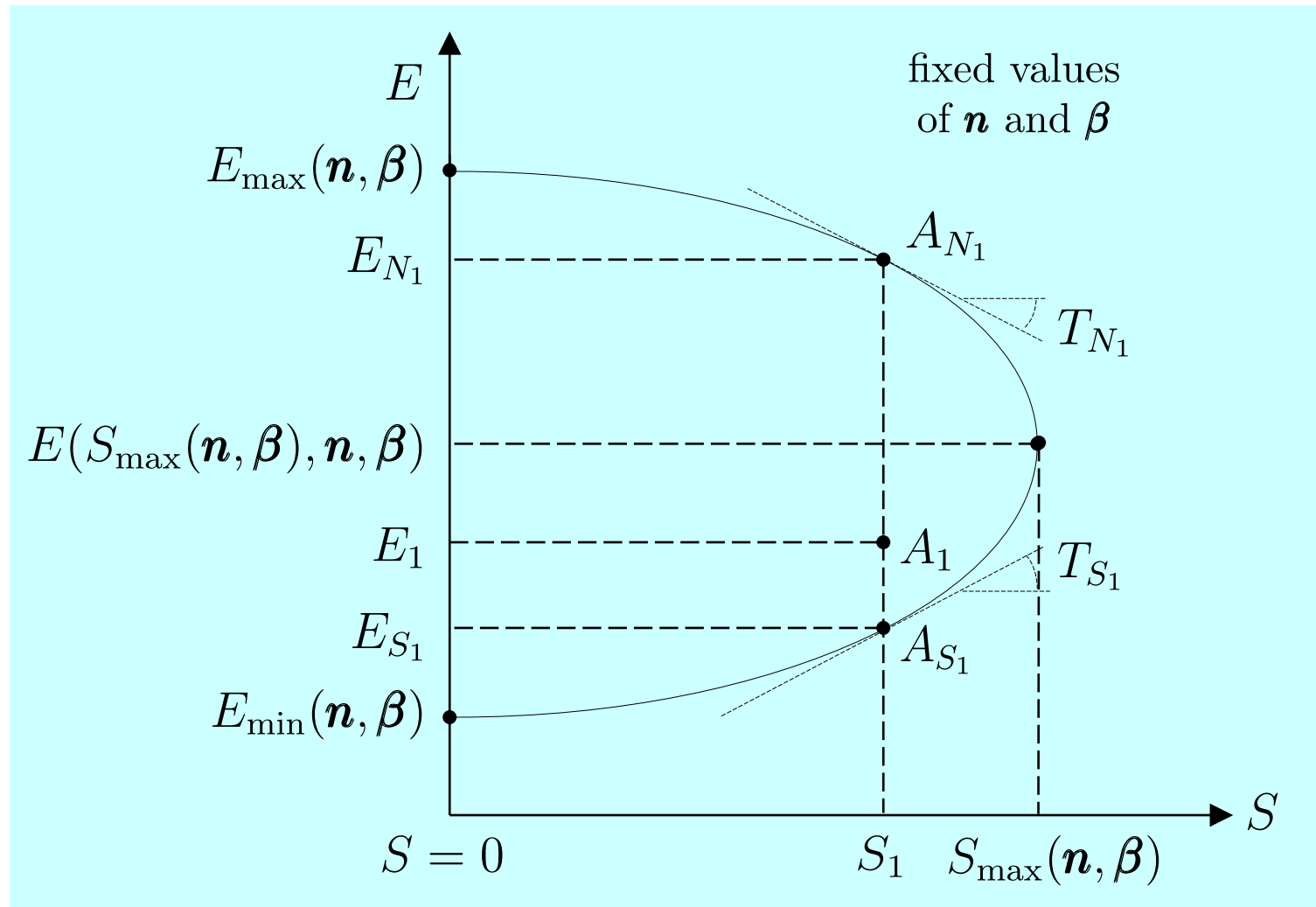
Representation of notSE states and SE states



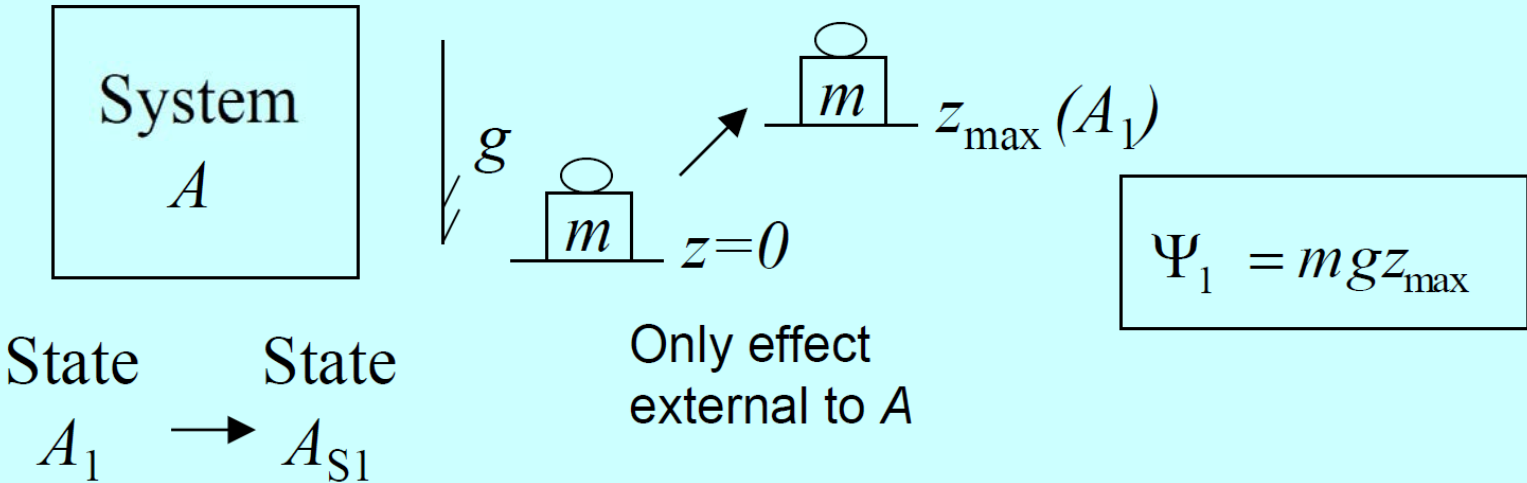
- A point in the region above the s.e.s. curve represents the projection of an infinite number of states that are not s.e.
- A point on the s.e.s. curve represents one and only one state, the unique s.e.s. with that value of the energy
- The slope of the tangent line to the s.e.s. curve is equal to the temperature of the s.e.s. represented by the point of contact
- Second Law and State Principle: for every value of E (horizontal line) there is a s.e.s. and it is the one with the maximum entropy
- The states considered by Mechanics are a subset of those considered by Thermodynamics, namely, those with zero entropy

Graphical representation of basic concepts on **Energy vs Entropy diagrams**:

Special systems with upper bounded energy



Review of basic concepts: **Consequences of First&Second Law:**
definition of property Adiabatic Availability



The **adiabatic availability** Ψ^R_1 of system A in state A_1 measures the maximum amount of energy that can be transferred from the system to a weight in a weight process for A starting from state A_1 .

Theorems: Adiabatic availability is a property, but it is NOT additive.

From the energy balance we obtain

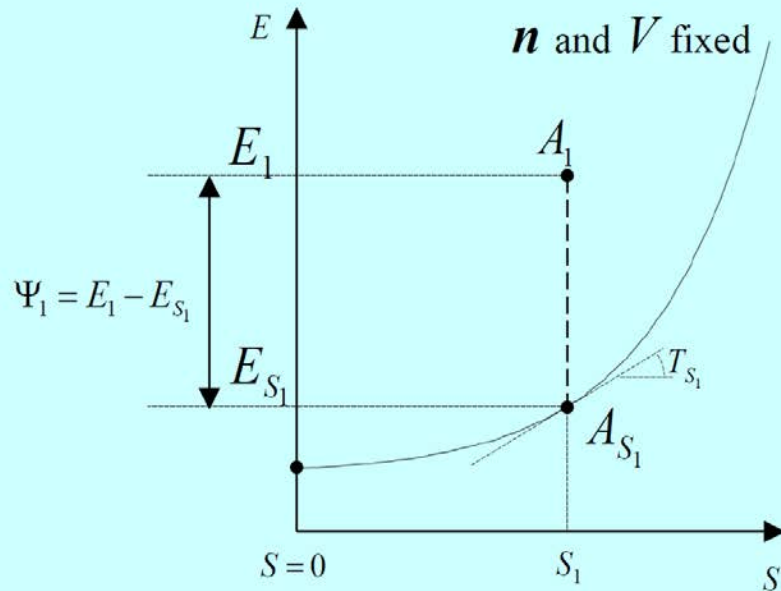
$$\Psi_1 = E_1 - E_{S1}$$

It is zero if and only if the state is stable equilibrium.

It obtains when the weight process is reversible and A ends in stable equilibrium. A unique stable equilibrium state A_{S1} can be reached in this way from state A_1 .

Graphical representation of basic concepts on **Energy vs Entropy diagrams:**

Adiabatic availability of notSE states



$$\Psi_1 = E_1 - E_{S_1}$$

Adiabatic availability (Ψ): it is the part of the energy of A in a given state A_1 which can be transferred to a weight with no other external effects. It is obtained by means of rev.w.p. which ends in a stable equilibrium state, A_{s_1}

- It is zero iff the state is a stable equilibrium state

Review of basic concepts: **Mutual equilibrium and definition of Thermal Reservoir**

Mutual stable equilibrium: Two systems A and B are in mutual stable equilibrium if their respective states are such that the composite system $C=AB$ is in a stable equilibrium state.

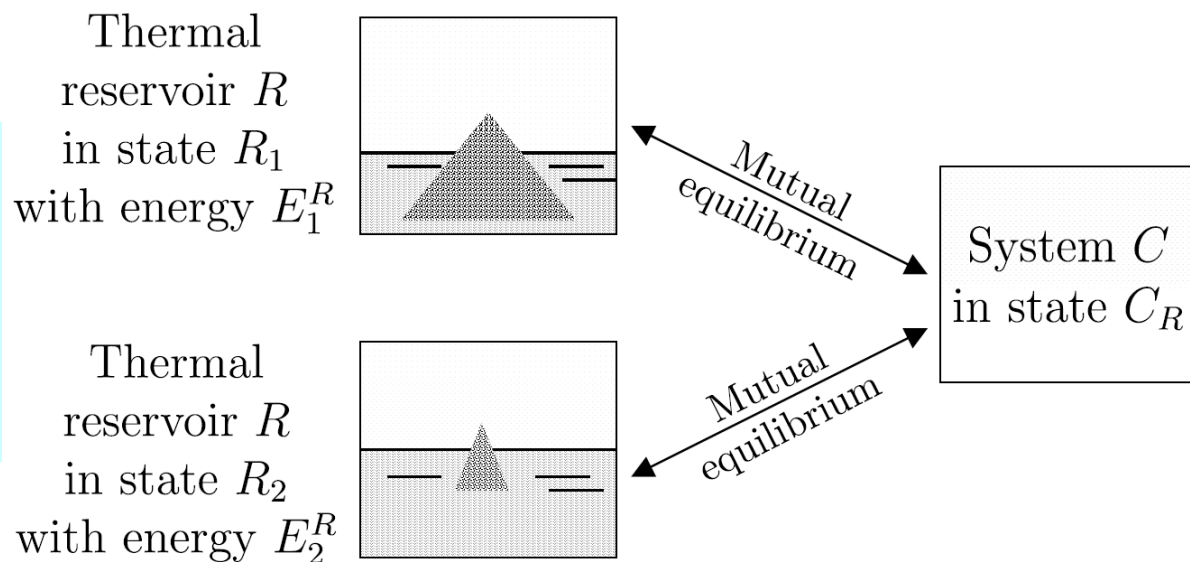
Thermal Reservoir (with constant amounts and parameters): a system R that in any of its stable equilibrium states is in mutual equilibrium with a given system C in a given state C_R

Example of a reservoir:

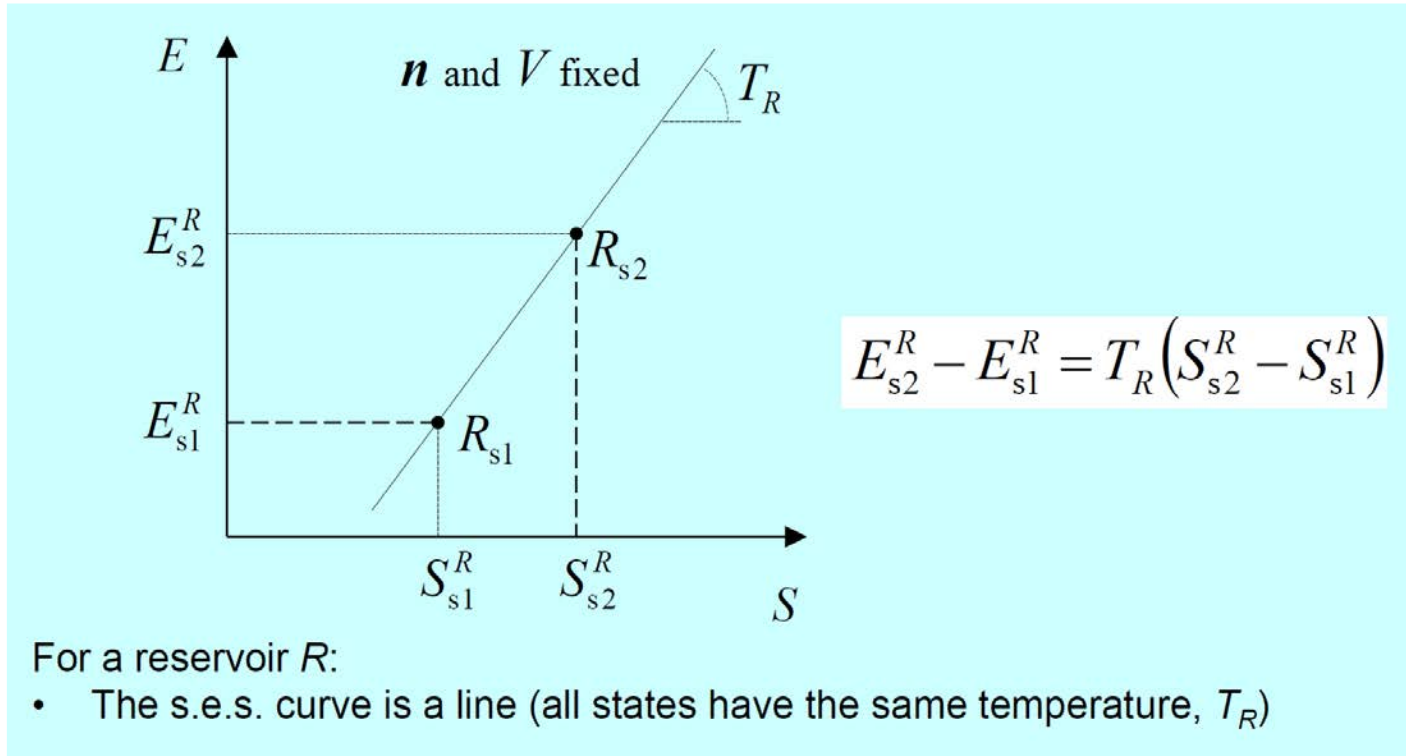
- H_2O at the triple point

$$T_{pt} = 273.16 \text{ K} \quad p_{pt} = 611.66 \text{ Pa}$$

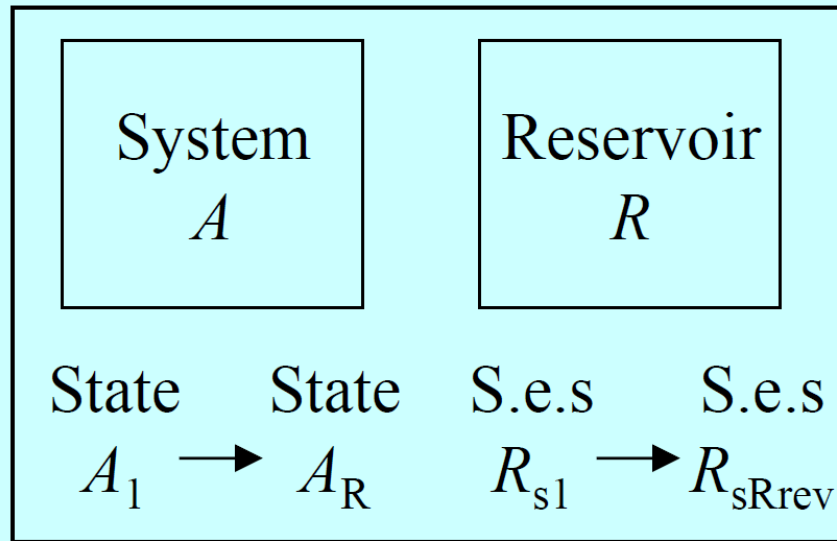
as long as all the three phases are present in a finite amount



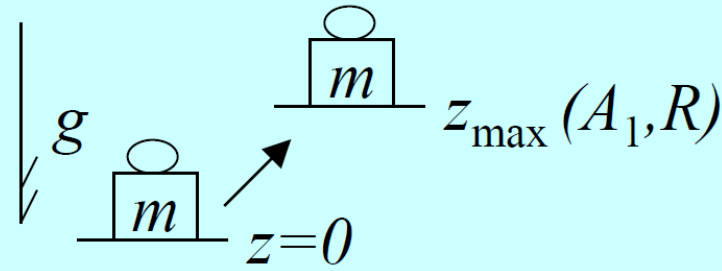
Graphical representation of basic concepts on **Energy vs Entropy diagrams:**
notSE and SE states of a thermal reservoir



Review of basic concepts: **Consequences of the (First&)Second Law:**
definition of Available Energy w.r.to a thermal reservoir



Max weight lift in a std. w.p. for AR :



Given state A_1 and the reservoir R , the **maximum weight lift** obtains when A ends in state A_R (mutual equilibrium with R) and the standard weight process for AR is reversible.

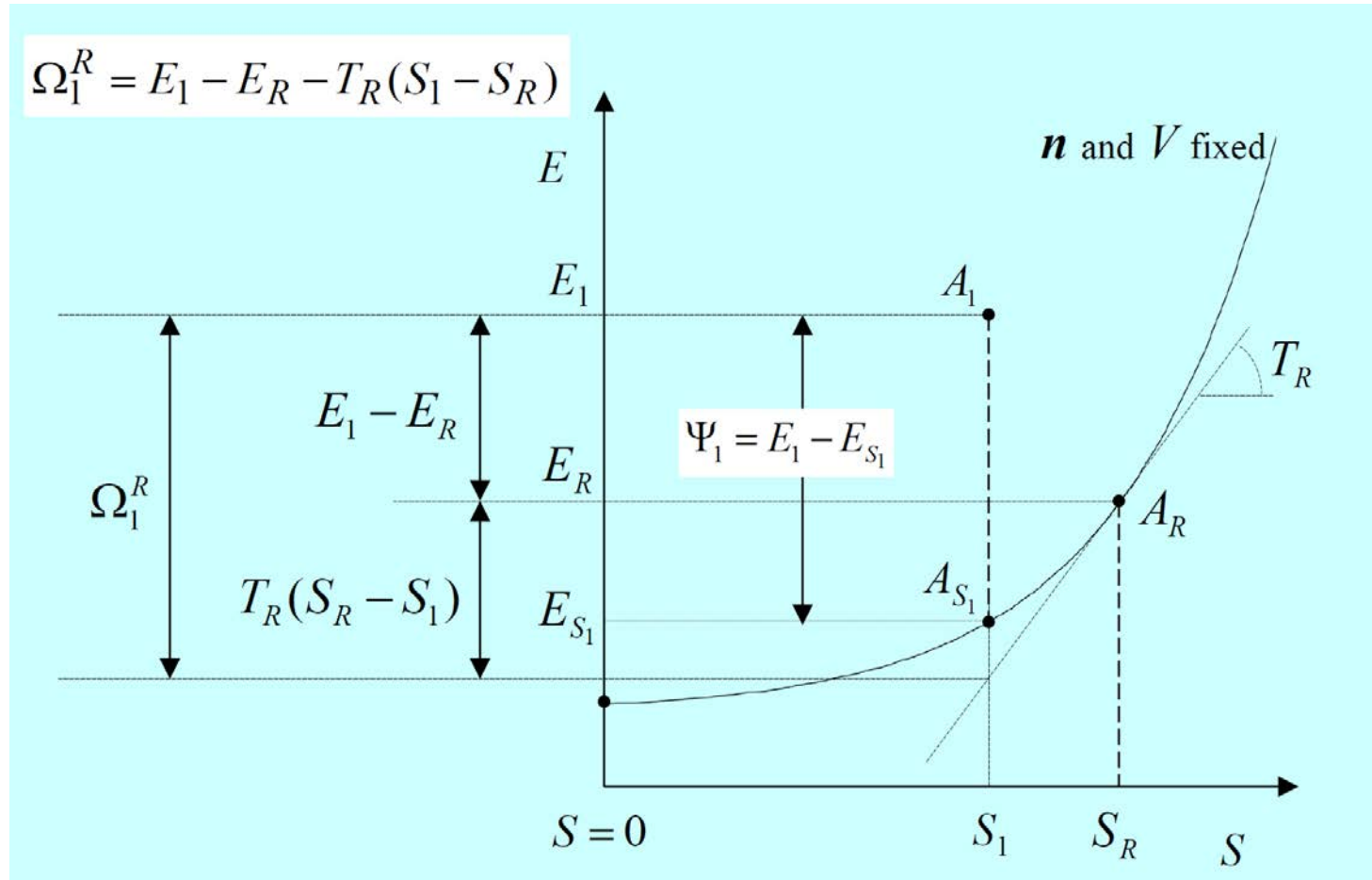
We denote the energy transferred to the weight by Ω_1^R from the energy balance

$$\Omega_1^R = mgz_{\max} = (E_1 - E_R) + (E_{s1}^R - E_{sRrev}^R)$$

and we call it the **available energy** of A in state A_1 **with respect to reservoir R** . From the definition of entropy, choosing state A_R as the reference state A_0 ,

$$S_1 = S_R + \frac{E_{sRrev}^R - E_{s1}^R}{T_R} \quad \longrightarrow \quad \Omega_1^R = (E_1 - E_R) - T_R(S_1 - S_R)$$

Graphical representation of basic concepts on **Energy vs Entropy diagrams:**
Available energy with respect to a thermal reservoir

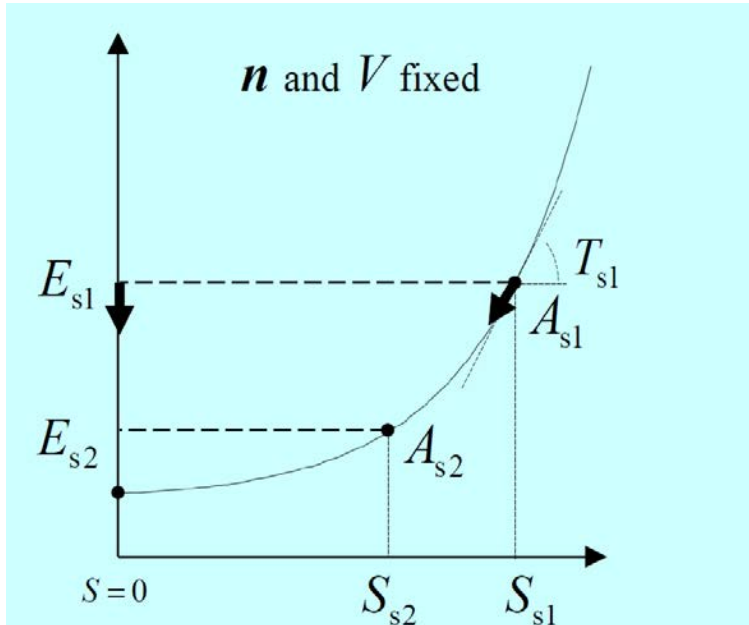


Graphical representation of basic concepts on **Energy vs Entropy diagrams:**

a system in a SES cannot

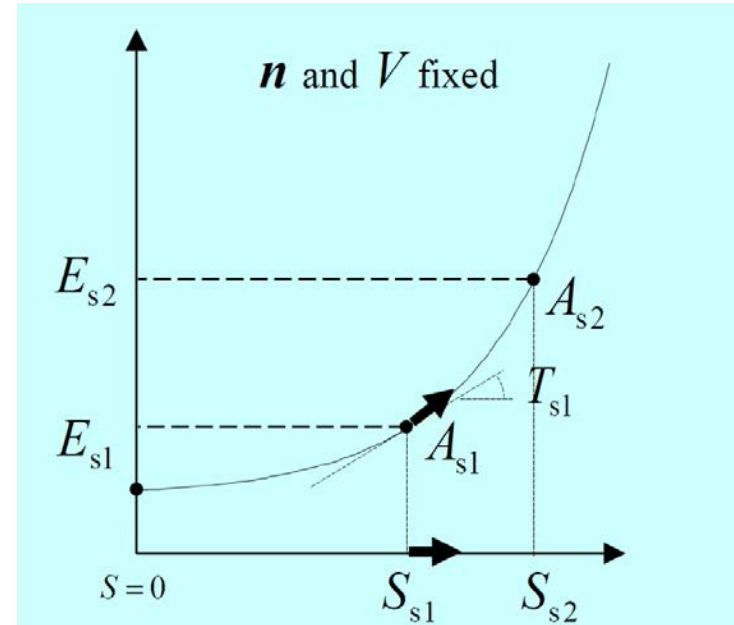
release energy unless...

receive entropy unless...



To extract energy from a system in a s.e.s., we must also extract entropy

$$S_{s1} - S_{s2} > (E_{s1} - E_{s2})/T_{s1}$$



To give entropy to a system in a s.e.s., we must also give energy

$$E_{s2} - E_{s1} > T_{s1}(S_{s2} - S_{s1})$$

Next:

Necessary conditions for mutual equilibrium

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