

hw #8 solution

(a)  $m_a = \eta_v \left( \frac{P}{RT} \right) V_D \frac{N}{z} = 0.8 \left( \frac{2.5 \times 10^5}{287 \times 393} \right) 1.29 \times 10^{-2} \times \frac{2000}{120} = 0.381 \text{ kg/s} = \underline{\underline{381 \text{ g/s}}}$

$m_{if} = \text{bsfc} \times P = \frac{200 \times 294}{3600} = \underline{\underline{16.3 \text{ g/s}}}$

$MF = m_a / m_{if} = 381 / 16.3 = \underline{\underline{23.3}}$

(b)  $m_a = m_a / (\eta N/2)$ ; where  $\eta = \# \text{ of cylinders} = 6$  A large drop!  
 $= \frac{381}{6 \times \frac{2000}{120}} = \underline{\underline{3.81 \text{ g}}}$

$m_f = m_a / (A/F) = \underline{\underline{0.163 \text{ g}}}$ ;  $V_f = \frac{m_f}{\rho_f} = \left( \frac{0.163}{0.78} \right) = \underline{\underline{0.21 \text{ cc}}}$

(c) Denote nozzle properties by subscript z.

$V_z = \frac{V_f}{\eta_z A_z \tau}$        $\eta_z = \# \text{ of nozzle holes} = 8$   
 $A_z = \text{hole area}$   
 $\tau = \text{inj duration:}$   
 $= \frac{0.21 \times 10^{-6}}{8 \times \frac{\pi (0.2 \times 10^{-3})^2}{4} \times 3 \times 10^3}$       at 2000 rpm  $\rightarrow 12^\circ \text{CA/ms}$   
 $40^\circ \text{CA} \Rightarrow \tau = 40/12 = 3.3 \text{ ms}$   
 $= \underline{\underline{253 \text{ m/s}}}$

(d) Reynolds no  $= \frac{\rho_f V_z d_z}{\mu} = \frac{253 \times 0.78 \times 10^3 \times 0.2 \times 10^{-3}}{5 \times 10^{-4}} = 7.9 \times 10^4 \text{ turbulent.}$

From Moody chart, friction coeff.  $f = 0.018$

$\Delta p_z = \frac{1}{2} \rho_f V_z^2 f \left( \frac{L}{D} \right)_z = \frac{1}{2} \times 0.78 \times 10^3 \times (253)^2 \times 0.018 \times 10 = \underline{\underline{45 \text{ bar}}}$

This is not significant (~3%) compared to the pressure drop of 1350 bar across the nozzle.

(e) Discharge coeff.  $C_d = \frac{V_z}{\sqrt{2 \Delta p / \rho_f}} = \frac{253}{\sqrt{2 (1350 \times 10^5) / 0.78 \times 10^3}} = \underline{\underline{0.43}}$

(f) Droplet Diameter  $d = (V_f)_{\text{inertial}} \frac{\sigma}{\rho_f V_z^2} = 30 \frac{0.025}{\left( \frac{50 \times 10^5}{287 \times 2000} \right) (253)^2} = \underline{\underline{0.54 \mu\text{m}}}$

(g)  $N_{\text{drop}} = \left( \frac{V_f}{\pi d^3 / 6} \right) = \frac{0.21 \times 10^{-6}}{\pi (0.54 \times 10^{-6})^3 / 6} = \underline{\underline{2.5 \times 10^{12} \text{ drops}}}$

Droplet spacing  $= (V_c / N)^{1/3}$ ;  $V_c = \frac{V_D}{N_c} = \frac{12.9 \times 10^6}{6 (16.5)} = 139 \text{ cc}$

Spacing  $= \left( \frac{139 \times 10^{-6}}{2.5 \times 10^{12}} \right)^{1/3} = 3.8 \times 10^{-6} \text{ m} = \underline{\underline{3.8 \mu\text{m}}}$

Thus each drop has to wrap and mix with air of  $\left( \frac{3.8}{0.54} \right)^3 = 398 \text{ times its size.}$   
A difficult job

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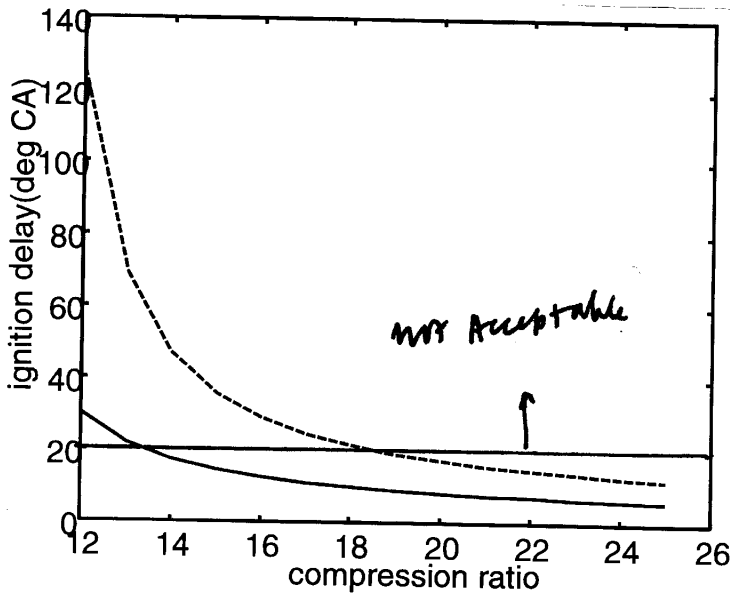
Ignition delay:

$$\tau (CA) = (0.36 + 0.22 \bar{S}_p) \exp \left\{ E_a \left[ \frac{1}{RT} \right] - \frac{1}{17190} \right\} + \left( \frac{21.2}{P-124} \right)^{0.63}$$

$$E_a = 618840 / (CA + 25)$$

$$T = T_i (CA)^{n-1} ; P = P_i (CR)^m$$

Results:



CR	ign delay (a)	ign delay (b)	in °CA
12.00	30.34	125.73	
13.00	22.15	69.04	
14.00	17.56	47.10	
15.00	14.64	35.88	
16.00	12.64	29.18	
17.00	11.17	24.76	
18.00	10.05	21.63	
19.00	9.17	19.30	
20.00	8.46	17.50	
21.00	7.87	16.07	
22.00	7.38	14.90	
23.00	6.96	13.93	
24.00	6.59	13.11	
25.00	6.28	12.40	

To have  $\tau_{id} \leq 20^\circ CA$

For the larger truck engine, the minimum compression ratio is 14.

For the small passenger car engine, the minimum is 19.

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8.3) Mass Diffusivity  $D = 1.8 \times 10^{-5} \left(\frac{p_0}{p}\right) \left(\frac{T}{T_0}\right)^{1.81}$   
 (m<sup>2</sup>/s)

Diffusion time  $\tau_{diff} = d^2/D$

Conditions	(a)	(b)	(c)
p (bar)	100	70	30
T (K)	2500	2000	1400
D (m <sup>2</sup> /s)	$8.36 \times 10^{-6}$	$2.97 \times 10^{-6}$	$9.75 \times 10^{-6}$
$\tau_{diff} - 10 \text{ nm}$	$1.2 \times 10^{-11} \text{ s}$	$1.35 \times 10^{-11} \text{ s}$	$1.03 \times 10^{-11} \text{ s}$
$\tau_{diff} - 100 \text{ nm}$	$1.2 \times 10^{-9} \text{ s}$	$1.25 \times 10^{-9} \text{ s}$	$1.03 \times 10^{-9} \text{ s}$
$\tau_{diff} - 1000 \text{ nm}$	$1.2 \times 10^{-7} \text{ s}$	$1.25 \times 10^{-7} \text{ s}$	$1.03 \times 10^{-7} \text{ s}$

} All small values compared to oxidation time

Oxidation time  
 mass conservation  $\rho(4\pi r^2) \frac{dr}{dt} = -(4\pi r^2)w$   
 $\Rightarrow \frac{dr}{dt} = -\frac{w}{\rho}$

integrating  $r - r_0 = -\frac{w}{\rho}t$ ; time to oxidize particle of radius  $r_0$  is  $t_0 = \frac{r_0 w}{\rho}$  — The time is proportional to  $r_0$ .

For the Nagle-Strickland Constable formula,  $p_{O_2} = p \cdot x_{O_2}$  thus the numerical values are: (for 100 nm = 0.1 μm diameter particle)

oxidation time (s) for 0.1 micron soot				
T(k)	p(bar)	time@x <sub>o2</sub> =0.1%	1%	10%
2.5000e+003	1.0000e+002	1.5798e-002	1.9327e-003	6.9704e-004
2.0000e+003	7.0000e+001	8.8868e-003	4.9975e-003	4.6617e-003
1.4000e+003	3.0000e+001	2.5396e-001	1.9351e-001	1.8747e-001

Note the sensitivity to temperatures. Sufficient O<sub>2</sub> has to be mixed in early (at high T) to oxidize the soot.

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2.61 Internal Combustion Engines  
Spring 2017

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