

# Model Solutions to 3.53 Problem Set 3

5.5. In answering this question, one can follow the procedure of Section 5.4.4. For



$$E = E_{M^{n+}, M(\text{solid})}^{\circ} + \frac{RT}{nF} \ln \frac{C_{M^{n+}}(0, t)}{C_{M(\text{solid})}(0, t)} = E_{M^{n+}, M(\text{solid})}^{\circ} + \frac{RT}{nF} \ln \frac{C_{M^{n+}}(0, t)}{1} \quad (2)$$

since  $a_M = 1$ , and which follows from equation (5.1.5). The following relations also apply

$$i(t) = nFam_{M^{n+}} [C_{M^{n+}}^* - C_{M^{n+}}(0, t)] \quad (3)$$

$$i_d(t) = nFam_{M^{n+}} C_{M^{n+}}^* \quad (4)$$

where  $m_{M^{n+}}$  is the mass transfer coefficient which replaces  $\sqrt{D_{M^{n+}}/\pi t}$  in equation (5.4.65) and  $i_d(t)$  follows from equation (5.2.11). Solving equation (3) for  $C_{M^{n+}}(0, t)$

$$C_{M^{n+}}(0, t) = C_{M^{n+}}^* - \frac{i(t)}{nFam_{M^{n+}}} \quad (5)$$

and equation (4) for  $C_{M^{n+}}^*$

$$C_{M^{n+}}^* = \frac{i_d(t)}{nFam_{M^{n+}}} \quad (6)$$

allows equation (5) to be written as

$$C_{M^{n+}}(0, t) = \frac{i_d - i(t)}{nFam_{M^{n+}}} \quad (7)$$

Substituting this result into equation (2) leads to

$$\begin{aligned} E &= E_{M^{n+}, M(\text{solid})}^{\circ} + \frac{RT}{nF} \ln \frac{i_d(t) - i(t)}{nFam_{M^{n+}}} \\ &= E_{M^{n+}, M(\text{solid})}^{\circ} - \frac{RT}{nF} \ln nFam_{M^{n+}} + \frac{RT}{nF} \ln(i_d(t) - i(t)) \end{aligned} \quad (8)$$

From Section 5.4.1(b), when

$$i(t) = \frac{i_d(t)}{2}, \text{ then } E = E_{1/2} \quad (9)$$

so that equation (8) may be rewritten

$$E_{1/2} = E_{M^{2+}, M_{(solid)}}^{\circ} - \frac{RT}{nF} \ln nFAm_{M^{2+}} + \frac{RT}{nF} \ln \frac{i_d(t)}{2} \quad (10)$$

which shows the relationship between  $E_{1/2}$  and  $i_d(t)$ . From equation (6)

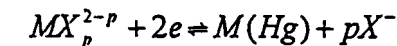
$$\frac{i_d(t)}{2} = nFAm_{M^{2+}} \frac{C_{M^{2+}}^*}{2} \quad (11)$$

which, when substituted into equation (10)

$$\begin{aligned} E_{1/2} &= E_{M^{2+}, M_{(solid)}}^{\circ} - \frac{RT}{nF} \ln nFAm_{M^{2+}} + \frac{RT}{nF} \ln nFAm_{M^{2+}} + \frac{RT}{nF} \ln \frac{C_{M^{2+}}^*}{2} \\ &= E_{M^{2+}, M_{(solid)}}^{\circ} + \frac{RT}{nF} \ln \frac{C_{M^{2+}}^*}{2} \end{aligned} \quad (12)$$

leads to the relationship between  $E_{1/2}$  and  $C_{M^{2+}}^*$ .

5.6. The system is analogous to that shown in equation (5.4.70).



(a) Given the conditions outlined after equation (5.4.70), equation (5.4.80) applies.

$$E_{1/2}^c = E_M^{\circ} - \frac{RT}{nF} \ln K_c - \frac{pRT}{nF} \ln C_X^* + \frac{RT}{nF} \ln \frac{m_A}{m_C}$$

A plot of  $E_{1/2}^c$  versus  $\ln C_X^*$  yields a slope of  $-\frac{pRT}{nF}$ . The intercept is equal to

$$E_M^{\circ} - \frac{RT}{2F} \ln K_C + \frac{RT}{nF} \ln \frac{m_A}{m_C}$$

Linear regression yields  $E_{1/2}^c = -0.0513 \times \ln C_X^* - 0.566$  with  $r = 0.99998$  for the data shown in the problem. Thus,  $-p = 2 \times 38.92V^{-1} \times -0.0513 = -3.99$ .  $p$  is 4.

(b) From equation (5.4.72),  $K_C = C_{MX_4} / C_M C_X^4$  is the formation constant for the reaction  $M^{2+} + 4X^- \rightleftharpoons MX_4$ . The stability constant is the same as  $K_C$ . From equation (5.4.82), one can solve for  $K_C$  as follows,

$$K_C = \exp \left\{ -\frac{nF}{RT} (E_{1/2}^c - E_{1/2}^M) - p \ln C_X^* \right\}$$

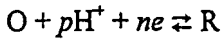
Because the diffusion coefficients are equal for the complex ion and the metal atom,  $m_A = m_C$ . An Excel spreadsheet can be set up as shown below.

n	2
p	4
F/RT(V <sup>-1</sup> )	38.92
E <sub>1/2,M</sub> (V)	0.081

$E_{1/2,C}(V)$	$nF(E_{1/2,C} - E_{1/2,M})/RT$	$C_X^*$	$\ln(C_X^*)$	$p \ln(C_X^*)$	$K_C$
-0.448	-41.17736	0.10	-2.30259	-9.21034	7.64012E+21
-0.531	-47.63808	0.50	-0.69315	-2.77259	7.81763E+21
-0.566	-50.36248	1.00	0	0	7.44984E+21

An average of the last column leads to a stability constant of  $7.6 \times 10^{21}$ . Alternatively, from equation (5.4.82), a plot of  $-nF(E_{1/2}^C - E_{1/2}^M)/RT$  versus  $\ln C_X^*$  leads to a slope of  $p$  and an intercept of  $\ln K_C$ . A linear regression of the data given leads to  $p = 3.993 \approx 4$  and  $\ln K_C = 50.38$  (with  $r = 0.99998$ ) or  $K_C = 7.58 \times 10^{21} = 7.6 \times 10^{21}$ , which agrees with the previous result.

**5.7 (a). The reversible reaction under consideration is**



The Nernst equation for this reaction follows from equation (5.1.5) and can be written as

$$E = E_{O,R}^o + \frac{RT}{nF} \ln \left[ \frac{C_O(0,t)C_{H^+}^p(0,t)}{C_R(0,t)} \right] \quad (1)$$

Proceeding as in Sections 5.5.3 and 5.5.4, the following equations can be written

$$i(t) = nFAm_O [C_O^* - C_O(0,t)] \quad (2)$$

$$i_d(t) = nFAm_O C_O^* \quad (3)$$

$$i(t) = nFAm_{H^+} [C_{H^+}^* - C_{H^+}(0,t)] \quad (4)$$

$$i(t) = nFAm_R [C_R(0,t) - C_R^*] = nFAm_R C_R(0,t) \quad (5)$$

The equality in the rightmost expression of equation (5) arises because species R is initially absent. Solving equations (2), (4), and (5), for  $C_O(0,t)$ ,  $C_{H^+}(0,t)$ , and  $C_R(0,t)$ , respectively leads to

$$C_O(0,t) = \frac{i_d(t) - i(t)}{nFAm_O} \quad (6)$$

$$C_{H^+}(0,t) = C_{H^+}^* - \frac{i(t)}{nFAm_{H^+}} \cong C_{H^+}^* \quad (\text{if } C_{H^+}^* \gg i(t)/nFAm_{H^+}) \quad (7)$$

$$C_R(0,t) = \frac{i(t)}{nFAm_R} \quad (8)$$

Substituting equations (6)-(8) into equation (1) leads to

$$E = E_{O,R}^o + \frac{RT}{nF} \ln \frac{m_R}{m_O} + \frac{pRT}{nF} \ln C_{H^+}^* + \ln \left[ \frac{i_d(t) - i(t)}{i(t)} \right] \quad (9)$$

which is the equation for the steady-state voltammogram of the reaction.

(b). When  $i(t) = i_d(t)/2$ , the last natural logarithm term of equation (9) is zero and equation (9) can then be recast as

$$E_{1/2} = E_{O,R}^{\circ} + \frac{RT}{nF} \ln \frac{m_R}{m_O} + \frac{pRT}{nF} \ln C_{H^+}^* \tag{10}$$

Then

$$\frac{dE_{1/2}}{d \ln C_{H^+}^*} = \frac{pRT}{nF} \tag{11}$$

or, at 25 °C,

$$\frac{dE_{1/2}}{d \log C_{H^+}^*} = 2.303 \frac{p}{n} \frac{8.31441 \text{ J mol}^{-1} \text{ K}^{-1} \times 298.15 \text{ K}}{96485 \text{ C mol}^{-1}} = 0.0592 \frac{p}{n} \tag{12}$$

which has units of volts. If  $\log C_{H^+}^* \approx -\text{pH}$ , then

$$\frac{dE_{1/2}}{d\text{pH}} = -0.0592 \frac{p}{n} \tag{13}$$

Experimentally, a plot of  $E_{1/2}$  as a function of pH will be linear with a slope of  $-0.0592p/n$  (units of volts) from which  $p$  can be determined.

5.13. The electrochemical reaction under consideration is



with only species  $\text{I}^-$  present initially. The key to deriving the shape of the sampled-current voltammogram that would be recorded at a stationary Pt microelectrode can be found in Section 5.4.3 where

$$i(t) = nF A m_R [C_R(0,t) - C_R^*] \tag{2}$$

When solved for  $C_R(0,t)$ , this becomes

$$C_R(0,t) = C_R^* + \frac{i(t)}{nF A m_R} \tag{3}$$

where  $m_R = (D_R/\pi)^{1/2}$ , as defined on page 185. Equation (3) can be written in terms of the diffusion limited current which follows from equation (1.4.17).

$$-\frac{i_d(t)}{C_R^*} = nF A m_R \tag{4}$$

This allows one to write

$$C_R(0,t) = C_R^* \left( \frac{i_d(t) - i(t)}{i_d(t)} \right) \tag{5}$$

The flux condition at the electrode surface is equivalent to equation (5.4.27), written as

$$3D_O^{1/2}C_O(0,t) + D_R^{1/2}C_R(0,t) = D_R^{1/2}C_R^* \tag{6}$$

where the factor of three accounts for the fact that the flux of I<sup>-</sup> is three times the flux of I<sub>3</sub><sup>-</sup>. Equation (6) leads to the following expression for C<sub>O</sub>(0,t) after substitution of equation (5).

$$C_O(0,t) = \frac{C_R^*}{3} \left( \frac{D_R}{D_O} \right)^{1/2} \left[ \frac{i(t)}{i_d(t)} \right] \tag{7}$$

The Nernst equation (5.4.1) is written as

$$E = E^{o'} + \frac{RT}{2F} \ln \left( \frac{C_O(0,t)}{C_R^3(0,t)} \right) \tag{8}$$

for reaction (1). Substituting for C<sub>O</sub>(0,t) and C<sub>R</sub>(0,t) from equations (5) and (7) respectively leads to

$$E = E^{o'} + \frac{RT}{4F} \ln \frac{D_R}{D_O} - \frac{RT}{F} \ln C_R^* - \frac{RT}{2F} \ln 3 + \frac{RT}{2F} \ln \left\{ \frac{i(t)i_d^2(t)}{[i_d(t) - i(t)]^3} \right\} \tag{9}$$

after some algebra. When  $i(t) = i_d(t)/2$ ,  $E = E_{1/2}$ , and equation (9) reduces to

$$E_{1/2} = E^{o'} + \frac{RT}{4F} \ln \frac{D_R}{D_O} - \frac{RT}{F} \ln C_R^* + \frac{RT}{2F} \ln \left( \frac{4}{3} \right) \tag{10}$$

Thus,  $E_{1/2}$  depends on the bulk concentration of species R or I<sup>-</sup>. Equations (9) and (10) are to be compared to equations (5.4.21) and (5.4.22) for the simpler  $O + ne \rightleftharpoons R$  case. One can immediately see that a plot of E vs  $\log [(i_d - i)/i]$  based on equations (9) and (10) would not be linear with a slope of 59.1/n mV at 25 °C. Moreover,  $E_{1/2}$  for the simpler reaction does not depend on concentration.